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Removal of microorganisms and their chemical metabolites from water using semiconductor photocatalysis

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Abstract.

Semiconductor photocatalysis has been applied to the remediation of an extensive range of chemical pollutants in water over the past 30 years. The application of this versatile technology for removal of micro-organisms and cyanotoxins has recently become an area that has also been the subject of extensive research particularly over the past decade. This paper considers recent research in the application of semiconductor photocatalysis for the treatment of water contaminated with pathogenic micro-organisms and cyanotoxins. The basic processes involved in photocatalysis are described and examples of recent research into the use of photocatalysis for the removal of a range of microorganisms are detailed. The paper concludes with a review of the key research on the application of this process for the removal of chemical metabolites generated from cyanobacteria.

Keywords: Photocatalysis, TiO₂, micro-organism, pathogen, disinfection, cyanobacteria, cyanotoxin.

1. Introduction

Since the first reported studies on the ability of titanium dioxide photocatalysis to destroy microbial pathogens in water [1-3], numerous studies have been undertaken to further the knowledge and understanding of this process [4-12]. Early insights into the bactericidal mechanism of action of TiO₂ photocatalysis were provided by Matsunaga *et al* [1] who demonstrated the direct oxidation of intracellular Coenzyme A in the bacteria *Lactobacillus acidophilus* and *E. coli* and in the yeast *Saccharomyces cerevisia*. This resulted in the inhibition of respiratory activity and eventual cell death. Later work by Saito *et al* [13] showed that cell death was accompanied by a rapid leakage of potassium ions along with the slow release of bacterial protein and RNA from *Streptococcus sobrinus* AHT. Results from transmission electron micrographs of treated *S. sobrinus* AHT showed that cell death was due to a significant disorder of cell membranes and cell wall decomposition. Further evidence for cell membrane involvement in the photocatalytic killing process was then demonstrated by several other groups [14-19].

This review will focus on recent developments in the area of photocatalytic destruction of microorganisms in water and on the challenges recent findings have presented for the real application of this technology to water treatment. In addition the use of semiconductor photocatalysis for the destruction of toxins released from cyanobacteria will also be considered. The World Health

Organisation (WHO) has stated that microbial hazards are the primary concern for drinking water quality in both developed and underdeveloped countries. The greatest risk is associated with the consumption of water contaminated with human or animal faeces as these are a source of pathogenic bacteria, viruses, fungi, protozoa and helminths. Therefore the use of any technology which can improve the quality of drinking water will provide significant worldwide health benefits [20].

2. Basic Processes in Semiconductor Photocatalysis

The basic principle of semiconductor photocatalysis relies on the formation of an electron-hole pair upon the absorption of a photon with energy equal or bigger than the semiconductor's band-gap. These two highly reactive entities are consequently involved in all subsequent coupled reactions oxidizing and reducing the suitable species in the system concomitantly.

The photogeneration of an exciton is a well established process both in direct and in indirect semiconductors [21]. Photogenerated electrons need to react with a proper acceptor, in environmental photocatalysis this is normally assumed to be O_2 forming initially a superoxide radical and finally ending up as H_2O , while the photogenerated holes, depending on their oxidizing power, are transferred to a mostly organic molecule inducing its oxidation. If this oxidation results in its complete degradation with the final products being CO_2 , H_2O and eventually ionized halides, the organic compound is said to be mineralized. Inorganic pollutants can as well be converted into less toxic or

less dangerous compounds [22, 23] by oxidation (reaction with holes) or reduction (reaction with electrons), while biological entities, e.g., macromolecules, bacteria, and viruses, can be killed or be removed entirely for disinfection.

The photocatalyst is therefore involved in the production of an oxidative and a reductive entity. In its first stage these are a photogenerated hole created in the valence band, h_{VB}^+ and a photogenerated electron formed in the conduction band, e_{CB}^- :

Independently from the way the h_{VB}^+ reach the surface, two different mechanisms may take place: (1) they are either transferred to the adsorbed pollutant causing its immediate oxidation (eq. 2), or (2) they are first transferred to adsorbed water molecules generating hydroxyl radicals, $\cdot OH$, which upon reaction with the pollutant will produce the respective oxidation products (eq. 3).

In eq. 3, the suffix "s" in $\cdot OH_s$ indicates the formation of surface groups and can thus be interpreted as surface trapped holes.

Mechanism 1 is normally regarded as direct oxidation or direct photocatalysis, while mechanism 2 is called indirect oxidation or indirect photocatalysis. Mechanism 1 is associated with systems where the pollutant adsorbs strongly at the photocatalyst surface establishing a good electronic contact, while mechanism 2 will be dominant in systems with a weak pollutant adsorption. The pollutant's photo-oxidation via mechanism 2 will therefore be mediated by the action of $\cdot OH_s$, and depending on how long the $\cdot OH_s$ need to migrate to meet the pollutant or how fast the latter can reach it, the photocatalytic oxidation rate will vary considerably. In principle, mechanism 2 can be as fast as mechanism 1, or it will be slower, but it is highly unlikely to be faster.

The photogenerated hydroxyl radicals can react while being adsorbed at the photocatalyst's surface, $\cdot OH_s$ (eq. 4), or after having been desorbed, i.e., acting as free hydroxyl radicals in solution, $\cdot OH_{free}$ (eq.5).

Systems in which the pollutant molecule is weakly adsorbed at the photocatalyst's surface are likely to be dominated by photocatalytic reactions

such as shown in eq. 4 or 5. Oxidation products will therefore be formed in the bulk liquid or gas phase, respectively, with a low probability of adsorption and eventual blocking or poisoning of the photocatalyst surface. This will be considerably different in systems where pollutants are strongly adsorbing. Photo-oxidation between two adsorbed species, i.e., $\cdot OH_s$ and $Pollutant_s$, surely demands a rather high surface mobility of these species, and cannot be disregarded since surface diffusion is considerably faster than diffusion from the bulk. Moreover, on nanoparticles the distances between $\cdot OH_s$ and $Pollutant_s$ might be small enough to allow electron transfer through tunnelling mechanisms.

Bahnemann et al, by means of time-resolved laser flash photolysis [24], identified two types of traps for holes: deep traps which are long-lived and unreactive and shallow traps in thermally activated equilibrium with h_{VB}^+ exhibiting a high oxidation potential. According to Monllor-Satoca et al [25], the unreactive deep traps might correspond to the intrinsic $\cdot OH_s$. In this case, the reactive shallow traps can be assigned to h_{VB}^+ , and in a similar manner as the direct hole transfer to adsorbed pollutants occurs, extrinsic $\cdot OH_s$ will be generated, since in both cases the adsorption occurs at unsaturated Ti surface atoms (eq. 2 and 3). Compounds that adsorb strongly on the surface of metal oxide particles usually form covalent bonds employing one, two, or three O atoms (to form mono-, bi- or three-dentate complexes) as it is the case for alcohols [26] and organic acids [27-29]. The reaction can be schematically described:

It should be noted, however, that the formation of $\cdot OH$ can as well follow a reductive pathway [30]:

with the e_{CB}^- converting the oxidant species, i.e., O_2 , into H_2O_2 which is then further reduced yielding hydroxyl radicals. Although H_2O_2 , should be formed as a rather stable product by the further reduction of $O_2^{\bullet-}$, it is only found in traces when working with TiO_2 powders [31], since by its subsequent reduction, very likely, $\cdot OH$ is formed.

In some systems mechanism 1 (eq. 2) appears to be uniquely responsible for the photocatalytic reaction, e.g., in the case of the photocatalytic degradation of formic acid [25], acetic acid [25], and oxalic acid [32]. Mechanism 2 (eq. 3) dominates other photocatalytic systems, e.g., the photooxidation of methanol [25], chloroform [25], methylviologen [25], 2-propanol [25], and phenol [25]. In some cases, both mechanisms can take place at the same time, for instance, depending on the illuminating photon flux, some systems may experience a transition from an indirect to a direct

mechanism, where a low photo flux favours an indirect mechanism and a high photon flux a direct one [25].

In general, regardless of the reaction in which the photogenerated charge carriers are involved, they are definitively leading to a complex set of subsequent reactions, resulting altogether in the so-called semiconductor photocatalytic activity. The photocatalytic reaction in a whole can proceed via several different mechanisms which may take place all at once, one after another, or some of them only in a few particular cases.

3. Photocatalytic Destruction of Micro-organisms

The usefulness of photocatalysis for the disinfection of water has been shown by the destructive effects it has on a wide range of microorganisms i.e. bacteria [33-43] viruses [44-47], fungi [48-52] and protozoa [53-55].

Many studies have examined the role of experimental variables on the response of microorganisms to photocatalytic treatment. These have included the effects of aeration, pH, chemical nature of bacterial suspension medium, photocatalyst type and concentration, light intensity and treatment time [39, 49, 55-62]. While these experimental parameters have been shown to affect microbial response to photo inactivation, consideration must also be given to the nature of the organism targeted. Some studies have shown that the response time of different microorganisms to photocatalytic inactivation is related to cell wall complexity. Microorganisms with a more complex cell wall have been shown to be more resistant to photocatalytic treatment. The

response of microorganisms to photocatalytic treatment has been reported to follow the order of protozoa being the most resistant followed by bacterial spores, mycobacteria, viruses, fungi and bacteria [61].

Furthermore the difference in cell wall complexity between gram positive and gram negative bacteria has also been shown to affect treatment time. Gram positive bacteria like enterococci require a longer treatment time than gram negative bacteria such as coliforms [59]. This is because gram positive bacteria have a very thick cell wall consisting of many layers of peptidoglycan and teichoic acids. On the other hand the cell wall of gram negative bacteria is very thin consisting of only a few layers of peptidoglycan surrounded by a second lipid membrane containing lipopolysaccharides and lipoproteins.

In addition some disease causing bacterial species can produce highly resistant structures known as endospores (spores), the role of which is to enable the bacteria to withstand unfavourable conditions. Spores are more resistant to physical destruction e.g. heat, radiation and desiccation, than vegetative cells. Consequently they require longer treatment time to be destroyed by photocatalytic means. Indeed many successful reports on the destruction of bacterial spores have come from studies which have employed additional ways of improving photocatalytic efficiency [35, 63, 64]. Dunlop *et al* [63] showed that electrochemically assisted photocatalytic disinfection significantly increased the rate of disinfection of *Clostridium perfringens* spores compared to open circuit conditions. Polo-López *et al* [65] highlighted

that, as with vegetative cells, differences in external spore wall structure have an impact on the response of microbial spores to photocatalytic treatment. They demonstrated a direct correlation between the sensitivity of *Fusarium spp.* spores to photocatalytic treatment and external spore wall complexity. The most complex spores, chlamydospores were shown to be the most resistant to treatment, followed by macroconidia and finally microconidia.

The impact of bacterial factors such as expression of cell surface structures and enzymes should not be overlooked when considering variables that affect the microbial response to photocatalytic treatment. Leung *et al* [43] examined the photocatalytic disinfection of the marine bacteria *Alteromonas alvinellae* and *Photobacterium phosphoreum*. *P. phosphoreum* was shown to be less susceptible than *A. alvinellae* to photocatalytic treatment which authors stated was related to differences in their fatty acid profiles and levels of superoxide dismutase (SOD) and catalase (CAT). SOD and CAT are bacterial intracellular enzymes which have a role in protecting bacteria from oxidative stress induced by their environment. The authors stated that higher SOD and CAT levels implied bacteria could defend themselves against .OH attack from photocatalysis to a greater extent.

Despite the number of studies undertaken to elucidate the mechanism of photocatalytic disinfection, the exact mode of action is yet to be shown. The antibacterial properties of TiO₂ photocatalysis are due to the generation of reactive oxygen species of which hydroxyl radicals are considered to be the

most important. The accepted sequence of events which take place when microorganisms undergo TiO_2 photocatalytic attack are thought to be cell wall damage followed by cytoplasmic membrane damage leading to a direct intracellular attack. Recently more sophisticated methods have been used to give further insight into this mechanism [67-70]. Goulhen-Chollet *et al* [70] used a biochemical approach to assess this mode of action of TiO_2 photocatalysis. Using 1D and 2D sodium dodecyl sulfate–polyacrylamide gel electrophoresis they showed that model proteins and bacterial proteins were quickly degraded during photocatalytic treatment resulting in a loss of cell activity and eventual cell death. They did not find a particular protein target and suggested that this indicated that the development of bacterial resistance to this form of treatment was almost impossible. Wu *et al* [67] used scanning electron microscopy to investigate of cell morphology of *E. coli* treated with a PdO/TiON photocatalyst. While the surface of control bacteria remained continuous and free of any damage those irradiated with visible light in the presence of the catalyst showed damaged membranes containing pits and holes in their cell walls. More recently, Pigeot-Rémy *et al* [68] examined the morphological damage irradiated TiO_2 caused to *E. coli* K-12, using transmission electron microscopy (figure 1). Bacteria were no longer cultivable after 1.5 hr and membrane structure was disorganised at this point. They also observed the concomitant release of chemical by-products such as oxamic and oxalic acids as well as ammonium cations, sulfate and nitrate anions. They suggested that these results correlated with nucleic acid

damage and showed using electrophoresis that bacterial DNA and RNA had completely disappeared after 7 hr of photocatalytic treatment.

Figure 1.

When considering the application of this technology for the disinfection of real water it should be taken into consideration that the response of bacteria to photocatalytic treatment in laboratory water samples differs greatly from those in real water samples such as wastewater or river water [37, 56, 58, 60, 71, 72]. The presence of suspended solids dissolved inorganic ions and organic compounds (mainly humic substances) and dissolved oxygen are thought to affect the efficacy of photocatalysis [72]. The issue of bacterial regrowth following photocatalytic treatment has been addressed by several authors [37, 57, 73-75]. Not surprisingly there is some variation in the conclusions reached particularly when comparing laboratory water samples and natural water samples. Rincon and Pulgarin reported no bacterial regrowth following treatment of *E. coli* k12 contaminated water in a compound parabolic collector (CPC) reactor irradiated under direct sunlight. They stated that monitoring the bacterial population following treatment was very important since by-products photogenerated from organic matter naturally present in water or those present as a result of bacterial lysis could offer favourable conditions for bacterial regrowth [75]. Moreover this paper reported a residual disinfection effect in which the decrease in bacterial numbers continued in the dark after the phototreatment ceased (figure 2). This was suggested to be due to radicals and other oxidative species,

produced during phototreatment, inducing damage that continues to affect the bacteria in the dark.

Figure 2.

Alrousan *et al* [72] used immobilised nanoparticle TiO_2 films to show that deactivation rates of *E. coli* were significantly lower in surface water samples compared to distilled water. They found that the organic and inorganic content of surface water lead to a reduction in the rate of photocatalytic disinfection (compared to results for distilled water) with the greatest decrease caused by the presence of humic acid. Lydakis-Simantiris *et al* [59] examined the disinfection of natural spring water and secondary treated municipal wastewater by TiO_2 photocatalysis. As with other groups, this work showed that the gram positive bacteria (*Enterococcus spp.*) was much more resistant to photocatalytic treatment than the gram negative bacteria (total coliforms) however after 60 min irradiation time with 1g/L Degussa P25 TiO_2 , small numbers of both faecal pathogens survived. They suggest this persistence may be due to the presence of dead bacteria and their excreted intracellular components competing with live bacteria for photogenerated hydroxyl radicals and/or forming a screen to reduce light penetration.

In addition, bacteria present in natural water samples are likely to be at different stages of growth. Therefore the impact of bacteria growth phase on response to photocatalytic treatment must be taken into consideration during

experimental design to ensure the efficacy of bacterial inactivation by the photocatalytic process. Leung *et al* [43] investigated the susceptibility of mid-log, late-log and stationary phase cells of the marine bacteria *Alteromonas alvinellae* and *Photobacterium phosphoreum* to photocatalytic treatment. They showed that no significant difference was observed for inactivation of *P. phosphoreum* during the three growth stages. *A. alvinellae* on the other hand showed higher resistance to photocatalytic treatment in late-log phase, which the authors suggested was related to lower levels of SOD and CAT expression.

The use of solar irradiation to disinfect natural water sources enhances the attractiveness of this technology particularly for use in remote areas [49, 55, 60-62, 65, 75-78]. While solar irradiation has many advantages e.g. readily available, cost effective, it does suffer from the drawback of not being able to control irradiation output. Therefore on cloudy days, photocatalytic efficiency may be reduced. Sichel *et al* [49], however, looked at the dependence of solar water disinfection on solar irradiation conditions under natural sunlight. Using *E. coli* k-12 and the fungal pathogens *Fusarium solani* and *Fusarium anthophilum* they showed that once the minimum solar dose had been received, photocatalytic disinfection efficiency wasn't enhanced by any further increase in light intensity (figure 3).

Figure 3.

The use of TiO_2 in suspension requires that it be removed from the water after treatment in order that it can be reused. One way of addressing this problem is by the use of immobilised or fixed catalyst systems. Moreover, studies have shown that immobilized systems are stable and are therefore readily applicable for continuous water treatment systems [36, 78-82]. One drawback, however, with using immobilised catalysts is the longer time required to inactivate microorganisms compared with that for catalysts in suspension [78]. This is thought to be due to the reduced interaction between the catalyst surface and the target microorganism [78]. van Grieken *et al* [79] compared the photocatalytic disinfection capability of a TiO_2 slurry and immobilised in an annular reactor. Using *E. coli* as a model organism they showed that while the immobilised system showed a lower disinfection activity than the slurry, the former was less inhibited by the presence of organic matter which leads to comparable irradiation times required for bacterial inactivation in wastewater effluent. Gomes *et al* [78] investigated the inactivation of *E. coli* under natural sunlight in suspension or supported on Ahlstrom paper fixed around concentric tubes inside a photoreactor and showed that inactivation was more efficient with suspended TiO_2 . They suggested that the interaction between the bacteria and the supported TiO_2 was the reaction constraint, reducing significantly the bacteria inactivation, as indicated by the values of the pseudo-adsorption constants. In addition the release of organic matter from the paper support was also responsible by the absorption of UV light, radical scavenging and inhibition of the catalyst as well as possibly acting as a nutrient supply for the bacteria Pablos *et al* [80]

used epifluorescence microscopy to highlight mechanistic differences in bacteria-catalyst interaction between immobilised and fixed TiO₂. They showed that while the irradiation time required to achieve total bacterial inactivation was comparable for both systems, the slurry system showed a higher inactivation rate at the beginning of the reaction that decreases progressively, whereas with the fixed-bed reactor the inactivation rate increased with increasing irradiation time. They suggested that this mechanistic difference made the immobilised system a more attractive option for scaling up the photocatalytic disinfection technology.

Since the activation of TiO₂ is limited by a narrow wavelength spectrum, much research has been undertaken into ways of augmenting photocatalytic activity to enhance this activity. This has included the use of dopants, the application of an electric current and the addition of H₂O₂. Dopants are metal ions that can shift absorption of the photocatalyst to the visible region, the advantage of which is that it negates the use of UV light. Many studies have shown that doping has produced effective photocatalysts capable of destroying pathogenic microorganism under visible light [83-87]. Rengifo-Rengifo- Herrera *et al* [83] showed that N, S co-doped Degussa P-25 powders were very effective in inactivating *E. coli* using visible light (figure 4). They suggested that the electron photo-promoted from the localized N and S states was the charge carrier responsible of the ROS formation. The main oxidative species were suggested to be the superoxide radical (O₂⁻) and singlet oxygen (¹O₂).

Figure 4.

Other effective dopants include copper [84], palladium oxide [67], platinum [86] and silver [36,46, 87]. Liga *et al* [46] showed that silver doping of TiO₂ nanoparticles significantly enhanced bacteriophage MS2 inactivation and that the inactivation rate increased with silver content. While van Grieken *et al* [36] showed that although the incorporation of silver into Degussa TiO₂ powder increased the disinfection efficiency of *E. coli*, this increase in activity was not due to an enhanced photocatalytic mechanism but rather it was the result of the bactericidal role of silver. Recently Kowal *et al* [87] showed that doping titania with silver provided an anti-MRSA and anti-MSSA effect without an exposure to UV radiation.

Many studies have reported that the addition of H₂O₂ [56, 74, 75] greatly enhances photocatalytic efficiency. Rincon and Pulgarin [74, 75] showed that the addition of Fe³⁺ and Fe³⁺/H₂O₂ resulted in improved rates of disinfection of water contaminated with *E. coli* K12 in a CPC reactor using solar irradiation and no bacterial regrowth was detected during the subsequent 24 hr period in the dark. Several studies have made use of the process of photoelectrocatalysis i.e. a process that combines electrochemistry with photocatalysis to effectively suppress the recombination of photoelectrons and holes and enhance photocatalytic disinfection efficiency [47, 88 - 91]. Baram *et al* [88] showed that electrochemically assisted solar photocatalysis efficiently destroyed *E. coli* after only 10 minutes treatment time. Li *et al* [91] showed that photoelectrocatalysis (performed under a +0.30 V (vs. Ag/AgCl) applied potential bias) was more effective in destroying *E.coli* than

photocatalysis alone. Cho *et al* [47] recently examined the inactivation of MS-2 bacteriophage in a TiO₂ photoelectrocatalytic system. They showed that the application of anodic potential to TiO₂ greatly enhanced inactivation of MS-2 and *Cryptosporidium parvum* oocyst as well as a range of gram positive and gram negative bacteria. They found that applying a positive potential also reactive oxygen species production.

The World Health Organization has stated that securing the microbial safety of drinking-water supplies is increased if multiple barriers are in place. These include the protection of water resources, proper selection and operation of a series of treatment steps and management of distribution systems to maintain and protect treated water quality. While the application of titanium dioxide photocatalysis as an additional barrier in this process is a real possibility there is still much work to be done in this area to ensure the reliability and efficacy of this process.

Table 1 gives an overview of the main microorganisms that have been studied in the past five years

4. Photocatalytic Destruction of Cyanotoxins

In addition to the challenges of pathogenic micro-organisms contaminating water there has been a growing problem in terms of the occurrence of cyanobacterial blooms, resulting from factors such as increased nutrient levels in water from intensive farming [92,93]. There are a number of genera of cyanobacteria including *Microcystis*, *Oscillatoria*, *Anabaena* and

Aphanizomenon which generated neurotoxins including anatoxin-a, anatoxin-a(s) and saxitoxins or hepatotoxins such as microcystins or nodularin. The heptapeptide Microcystins are heptapeptides and over 60 congeners have been detected (figure 5). Microcystins primarily known as potent inhibitors of serine/threonine protein phosphatase 1 (PP1), PP2A, PP3 and PP4 [94-96]. At higher doses microcystins cause acute hepatic failure and were associated with the death of patients undergoing dialysis in Brazil in 1996 [97]. In addition to microcystins cylindrospermopsin was also detected in the contaminated water. As a result of the concern of the potential tumour promoting activity of microcystins and the World Health Organisation have published of a Guideline Value for microcystins of $1 \mu\text{g dm}^{-3}$ in potable water. Microcystins are however very stable molecules and it has been suggested that conventional water treatment systems may be undependable for the elimination of these toxins from potable water [98-100].

Figure 5.

The application of semiconductor photocatalysis for the removal of cyanotoxins has been comprehensively investigated since the first report in 1997 [101]. Using a P25 material a rapid destruction of microcystin-LR was achieved [101]. The photocatalytic decomposition process was found to depend on a number of parameters including toxin concentration, pH and light intensity [102].

In a subsequent study, Robertson *et al*, reported that when the

photocatalytic decomposition reaction was performed in heavy water, a kinetic solvent isotope effect of approximately 3 was obtained (Figure 6) [103]. In addition a number of hydroxylated products were detected using mass spectrometry. This result suggested that the primary mode of attack on the microcystin was via hydroxyl radicals generated on the titanium dioxide surface. In this paper it is also reported that no photocatalytic degradation proceeded under a nitrogen atmosphere.

Figure 6

The mechanism of the photocatalytic destruction of microcystin was studied in more detail by Lawton *et al* who studied the decomposition products using liquid chromatography [104]. In this paper a total of seven UV detectable products were generated as part of the photocatalytic reaction. Six of these products, however, did not undergo further decomposition on continued photocatalysis. In total only 10% of the microcystin was completely mineralised. The toxicity of the by-products was consequently assessed using both brine shrimp and protein phosphatase bioassays [105]. No residual toxicity was detected using either bioassay on extended photocatalysis (figure 7).

Figure 7.

Antoniou *et al* studied the photocatalytic oxidation of microcystin-LR on transparent thin TiO₂ films [106]. Specifically they investigated the effect of pH, toxin concentration, TiO₂ coated film surface area and film structural properties on the rate of toxin destruction. The best performance for toxin destruction was achieved using a 0.3 µM coating under both acidic and neutral pH conditions. Protein phosphatase bioassay demonstrated that removal of microcystin-LR toxicity had been achieved. Although acidic pH favoured the photocatalytic decomposition of the microcystins, it was reported that acidic pH limited the available sites of the toxin for degradation to the diene bonds of Adda and the double bond of MeAsp. Under neutral conditions, however, the methoxy and the aromatic groups of the Adda part of the microcystin structure were involved. Structures for the interaction of the microcystins and the TiO₂ photocatalyst, under acidic conditions, were proposed by Antoniou *et al* [106].

A more detailed assessment of the mechanism of the photocatalytic decomposition of microcystin-LR was performed by Liu *et al* using LCMS [107]. In this study it was reported that the destruction of the cyanotoxin was initiated by three major pathways. These were a UV transformation, hydroxyl radical attack and a direct oxidation of the substrate. Song *et al*. [108] demonstrated that the photoisomerisation of microcystin-LR could not be achieved using UVA light and UVC was required to induce this transformation. In a detailed study of the mechanism of the photocatalytic decomposition of microcystin, Antoniou *et al* [109] reported that the

mechanism of the addition of hydroxyl radicals to the diene bonds could induce this isomerisation.

Antoniou *et al* [109, 110] studied the reaction intermediates generated in the photocatalytic destruction of microcystin-LR using TiO₂ photocatalysts immobilised to glass [109] and stainless steel [110]. At pH 5.7 a total of eleven new intermediates were observed many of which were not reported in the study by Liu [107]. It was reported that acidic conditions were favoured in the photocatalytic destruction process. Furthermore with the lower surface area of the films compared to powder suspension the degradation rate was believed to be slower resulting in more intermediates being generated.

The decomposition of a series of different microcystin variants, -LR, -YR and -YA was subsequently described by Shepard *et al* [111]. Each of the variants was decomposed within 20 minutes and each process had a half life of less than 5 minutes.

Feitz *et al*. [112] studied the effect of pH on the photocatalytic degradation of microcystin-LR. It was found that this was greatest at a pH level of 3.5, a level at which dark adsorption was also at a maximum. A detailed study of the influence of pH on the photocatalytic destruction of a series of microcystins including microcystin-LR, -RR, -LW and -LF was described by Lawton *et al* [113]. It was reported that the initial rate of the cyanotoxin destruction was strongly influenced by the pH level and this correlated well with the corresponding level of dark adsorption. This influence was believed

to be due to a combination of effects including the hydrophobicity and overall charge of the microcystin variants. In addition the rates were believed to be influenced by the surface charge of the photocatalyst material as this varied around the point of zero charge for Degussa P25 TiO₂ at pH 6.25 which also affected the dark adsorption of the cyanotoxins.

The addition of additives such as hydrogen peroxide or ferrate has been demonstrated to have a positive enhancement on the photocatalytic decomposition of microcystins. Cornish *et al* [114] reported a significant improvement on the photocatalytic destruction of microcystin-LR when small quantities of hydrogen peroxide were added to the reaction matrix (figure 8). The overall effect was however strongly dependent on the quantity of peroxide added, with an ideal peroxide loading of between 0.005 and 0.1 % being reported. At peroxide concentrations above this level the rate of microcystin decomposition started to decline and it was believed this was due to a competitive adsorption of the peroxide with the toxin [114]. It was also reported that when peroxide was added fewer decomposition products were detected by liquid chromatography. Furthermore there was also a more rapid reduction in the toxicity of the treated water when peroxide was added as indicated by both brine shrimp and protein phosphatase bioassays [105].

Figure 8.

The photocatalytic destruction of microcystin-LR was also significantly enhanced by the addition of ferrate [115]. Up to 63% of a 2 mg l⁻¹ solution of microcystin was destroyed after 30 minutes photocatalysis, which was

reported to be 4.4 times greater than the level achieved in the absence of Fe ions. This process was also reported to be strongly dependent on pH level with this being maximised at pH 6.

Liu *et al* [116] reported the photocatalytic destruction of microcystin-LR on a number of commercially available TiO₂ powder (P25, PC50, PC500 and UV100) (figure 9) and granular (KO1, KO3, TiCat-C, TiCat-S) materials. Using liquid chromatography-mass spectrometry analysis it was established that the primary decomposition pathway of the cyanotoxin was the same for all the photocatalyst materials examined. This observation suggested that the physical properties of the catalysts had little influence on the photocatalytic degradation pathway of microcystin-LR.

One of the main challenges in developing a photocatalytic process that can be applied to large scale water treatment has been the development of a visible light absorbing photocatalyst. A nitrogen-doped TiO₂ visible light absorbing photocatalyst was used by Choi *et al* [117] in the destruction of microcystin-LR. Under irradiation of light at 420nm a 100% destruction of a 5mM microcystin-LR solution was achieved. Under the same experimental conditions only 10% toxin destruction was observed using a Degussa P25 photocatalyst. Pelaez *et al.* [118] utilised N-F-codoped TiO₂ nanoparticles for the photocatalytic destruction of microcystin-LR using visible light at 420 nm. This process was found to be most favourable at pH 3 where complete toxin destruction was achieved within 300 min. It was proposed that at this pH the

adsorption of the catalyst was maximised through and electrostatic interaction between the microcystin and the photocatalyst. The application of $\text{TiO}_2\text{-Pt}$ (IV), $\text{TiO}_2\text{-C}$, $\text{TiO}_2\text{-Rh}$ (III) materials, for the visible light photocatalytic degradation of microcystin-LR was reported by Graham et al. [119] The $\text{TiO}_2\text{-Rh}$ (III) proved to be the most effective material 100% of the toxin being decomposed with 60 minutes. The next most efficient materials were the platinum and carbon doped materials which destroyed 90% and 80% of the microcystin within 60 minutes respectively. Pelaez *et al* [120] investigated the effect of a range of water parameters in the degradation of microcystin-LR using the nitrogen and fluorine doped TiO_2 photocatalyst. These parameters included pH, alkalinity dissolved oxygen and naturally occurring organic materials (NOM) such as humic acid. As with previous reports the degradation was most efficient under acid conditions. Increasing concentrations of carbonate and NOM reduced the rate of destruction. Interestingly when natural water was spiked with microcystin and irradiated with artificial light at greater than 420nm no degradation of the toxin was observed. When a similar system was irradiated with sunlight over 90% of the toxin was removed within five hours irradiation. This was believed to be due to NOM acting as a photosensitiser for the solar photocatalytic degradation of the toxin. This observation may be supported by the observation by Robertson *et al* [121] who previously reported that the phycocyanin pigment generated by cyanobacteria were involved in the photosensitised degradation of microcystin-LR.

Less work has been reported on the removal of other cyanobacterial toxins from water. Nodularins are pentapeptide cyanotoxins produced by the cyanobacteria, *Nodularia spumigena*, they are tumour-promoters and their presence in drinking water is considered to play a role in the development of primary liver cancer in humans. It is therefore imperative that effective methods for their removal from drinking water sources are sought. TiO₂ photocatalysis has also been applied to the destruction of the, nodularin from water [122]. As was the case with microcystin-LR the nodularin was rapidly decomposed with the corresponding elimination in toxicity. The photocatalytic process also eliminated the major by-products of the decomposition process. This was demonstrated using LC-MS where all were detectible products completely degraded within 100 minutes photocatalysis. Again in a similar manner to the photocatalytic destruction of microcystin-LR, the major pathway of the photocatalytic decomposition process appeared to involve isomerisation, substitution and cleavage of the Adda conjugated diene structure in either nodularin or its resulting derivatives.

Cylindrospermopsin is a cyanotoxin produced by *Cylindrospermopsis raciborskii*. This organism is regularly found in reservoirs in SouthEast Queensland, Australia where its presence has resulted in the closure of these reservoirs [123]. Senogles *et al* [123] reported on the photocatalytic destruction of this toxin using two commercially available types of TiO₂; Degussa P25 and Hombikat UV-100. Using a cell free extract of

Cylindrospermopsis raciborskii the authors used HPLC-tandem mass spectrometry to assess the effect of several variables on response of toxin to photocatalytic destruction. Variables examined were pH, temperature, toxin concentration and dissolved organic carbon concentration. Overall Degussa P-25 was found to be the more efficient catalyst and pH was the experimental variable shown to have the greatest influence on toxin degradation, regardless of catalyst type. The highest rate of toxin degradation was observed with pH9, this is in contrast to findings for microcystin –LR destruction which has been reported to take place more effectively at low pH [113]. As with destruction of bacteria, differences in the photocatalytic destruction rates of cyanobacterial toxins in natural water samples and laboratory water have been reported [123]. Unlike bacteria, however, the presence of dissolved organic carbon has been reported to enhance destruction of cylindrospermopsin [123]. Senogles *et al* [123] suggested that the enhanced destruction of cell free extracts of *Cylindrospermopsis raciborskii* in spiked natural water compared with those in laboratory water where due to the presence of organic and inorganic matter in the natural water.

As with any photocatalytic reactor system, the use of fixed TiO₂ is preferable to TiO₂ in suspension to avoid the problem of slurry removal following water treatment. Anabaena (as well as microcystis) were successfully destroyed using TiO₂ coated Pyrex glass beads in the presence of UV light [124]. The

authors stated that this method could successfully be employed for the practical application in a eutrophicated river using natural sunlight.

In addition to toxin production, cyanobacteria also produce non-toxic compounds which can affect water quality. Geosmin (GSM) and 2-methylisoborneol (MIB) are bi-cyclic tertiary alcohols produced by cyanobacteria, which can taint water and fish and also give them an unpalatable earthy-musty flavour. It is therefore desirable that these compounds also be removed from drinking water supplies and in the aquaculture industry. Lawton *et al* [125] demonstrated the rapid destruction of MIB and GSM using TiO_2 photocatalysis, as measured by GC-MS. Using concentrations of both compounds representative of those found in the environment, a greater than 99 % reduction of both compounds was achieved within 60 min. irradiation time [125]. Yoon *et al* [128] highlighted the effectiveness of TiO_2 -entrapped EFAL (extra-framework-aluminium)-removed Y-zeolites (TiO_2 -EFAL-removed Y-zeolites) for removing taint compounds, such as 2-methylisoborneol (2-MIB), in water. Results of kinetic studies showed that TiO_2 -EFAL-removed Y-zeolites were highly adsorptive and had higher photocatalytic quantum efficiency than that of Degussa P-25 TiO_2 .

Marine algal toxins are responsible for huge economic losses in the fishing industry. Moreover most have deleterious effects on human health which often occurs following consumption of shellfish which have fed on the algae. Several studies have however reported on the effectiveness of TiO_2

photocatalysis in destroying these toxins. Djaoued *et al* [129] showed nanocrystalline titania thin films effectively degraded the marine neurotoxin, domoic acid. This toxin which is common in American coastal waters is particularly problematic in the shellfish and crustacean harvesting industry. During photocatalytic treatment the authors noted the presence, transformation and degradation of various isomers of domoic acid, as measured by HPLC.

One of the limiting factors of any photocatalytic reaction is the interaction of the catalyst with its target. Tominaga *et al* [130] produced a surface modified TiO₂ to study the degradation of the paralytic shellfish toxin; saxitoxin. The hybrid photocatalysts were developed by introducing molecular recognition sites to the surface of TiO₂ nanoparticles using a hydration-dehydration process or by silane coupling reaction and free radical polymerization (figure 1 from reference). Catalysts from both synthesis methods were shown to selectively degrade saxitoxins. The authors suggested it was the initial adsorption selectivity which affected toxin degradation rates. Brevetoxins are neurotoxins produced by the harmful marine algae *Karenia brevis*. Their presence in water is often indicated by the appearance of red tide which is the result of the release of photosynthetic coloured pigments from ruptured cells. Removal of brevetoxins from water sources using UV and solar photocatalysis has been examined by Khan *et al* [131]. Greatest toxin destruction was observed using UV light although sunlight was also effective. Furthermore as with most bacterial studies,

photocatalytic destruction was faster in laboratory water than in synthetic seawater, this was considered to be due to the presence of humic substances and other ions present in seawater which reduce the efficiency of photocatalytic degradation [131].

Table 2 summarises the range of metabolites that have been successfully destroyed using semiconductor photocatalysis.

5. Conclusions.

Semiconductor photocatalysis has proven to be an effective method for the removal of micro-organisms and cyanotoxins from water. Over the past decades there have been a number of attempts to develop an understanding of the precise mechanism of the photocatalytic oxidation of bacterial species. While significant progress has been made there is still much research that needs to be undertaken before the process is fully understood. With respect to cyanotoxins such as microcystins, TiO_2 photocatalysis has proven to be particularly effective compared to traditional water treatment processes such as activated carbon or chlorination. The main challenges that are limiting the wide scale adoption of this process as a practical water treatment process is the lack of commercially available visible light absorbing photocatalyst materials and to date the process has only been scaled to a pilot level. The development of an effective, commercially available, visible light absorbing photocatalyst will be an important step in assisting the scale-up of the photocatalytic water treatment process. The strong attenuation of UV light by

water, particularly natural waters contaminated by micro-organisms reduces the efficiency and hence increases the energy cost of photocatalytic water treatment. Visible light is less attenuated and also a greater portion of the sun's spectrum could be utilised enabling solar activated processes to be adopted. In order for this technology to be adopted as a practical water treatment process, ultimately it will be necessary to demonstrate the process is capable of treating thousands of m³ volumes per hour whether or not the system is activated by visible or UV light.

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Figure. 1 TEM pictures of *E. coli* cells in suspension in water exposed to UV-A photocatalysis with TiO₂ P-25 (0.25 g/l) and IUV-A = 3.45mW/cm²: (a) after 80 min of exposure, (b) and (c) after 180 min of exposure. (Reproduced from 41 with kind permission of Elsevier).

Figure 2. Evolution of *E. coli* in the dark after solar disinfection: without catalyst, experiment of September 20th (a), TiO₂/sunlight system experiment of September 15th (d), (Reproduced from 75 with kind permission of Elsevier).

Figure 3. Effect of the cumulative solar UV dose (bars with diagonal fill) and hourly average solar UV irradiance (solid bars) on the photocatalytic inactivation of *F. solani* under natural solar radiation with (●,○) and without TiO₂ (■,□). Experiments started at 08:30 (a) and at 10:15 (b). Initial concentration of *F. solani* 1.3 x 10³ CFU/mL. Each point represents the average of triplicates, and vertical lines show the statistical error at 95% confidence level. (Reproduced from 49 with kind permission of Elsevier)

Figure 4. Photocatalytic *E. coli* inactivation under visible light irradiation. (●) Pure Degussa P-25, (▲) pure Degussa P-25 annealed at 400 °C, (◆) N, S co-doped P-25 and (■) N-doped P-25, (×) visible light exposure without catalyst. pH 7.0, UV intensity 0.1Wm⁻² and visible light intensity: 60Wm⁻² (Reproduced from 83 with kind permission of Elsevier).

Figure 5. Generic structure of microcystins where X and Z represent the variable amino acids and, D-Me-Asp is D-*erythro*- β -methylaspartic acid, Adda is (2*S*, 3*S*, 8*S*, 9*S*)-3-amino-9-methoxy-2,6,8-trimethyl-10-phenyldeca-4(*E*),6(*E*)-dienoic acid, D-Glu is D-glutamic acid and Mdha is *N*-Me-dehydroalanine. (reproduced with permission from Environ. Sci. Technol. 37 (2003) 3215–3219. Copyright 2003 American Chemical Society).

Figure 6. The photocatalytic destruction of microcystin-LR in H₂O and D₂O solvents (Reproduced from 103 with kind permission of Elsevier)

Figure 7. Destruction and PP1 inhibition of microcystin-LR (photocatalysis with TiO₂). Each point plotted for PP1 inhibition is the mean of 3 observations. The concentration of PP1 in the test was 4 $\mu\text{g mL}^{-1}$. (reproduced from 105 with kind permission from Elsevier).

Figure. 8. Destruction of microcystin-LR by TiO₂ photocatalysis with ($\diamond$) 0.1% H₂O₂ and ($\square$) 0.01% H₂O₂. B corresponds to the toxin concentration before TiO₂ was added to the system. Levels monitored by HPLC, bars are equivalent to 1 SD ($n=2$). (reproduced from 114 with kind permission from Elsevier).

Figure 9. The photocatalytic degradation of Microcystin-LR on TiO₂ (P25, PC50, PC500 and UV100) over 100 min irradiation times (reproduced from 116 with kind permission from Elsevier).

Table 1. Range of micororganisms removed from water using semiconductor photocatalysis.

Table 2. Range of cyanobacterial metabolites removed from water using semiconductor photocatalysis

Figure 1

Figure 2.

Figure 3.

Figure 4.

Figure 5

Figure 6.

Figure 7

Figure 8.

Figure 9.

Table 1

Species	References
Bacteria	
Coliforms	58, 59
<i>Escherichia coli</i>	9, 10, 11, 12, 36, 37, 42, 45, 56, 57, 68, 72, 75, 78, 79, 86
<i>Salmonella spp.</i>	10
<i>Pseudomonas aeruginosa</i>	10
<i>Bacillus spp.</i>	40, 62, 64
<i>Clostridium perfringens</i>	35, 63
<i>Staphylococcus aureus</i>	52, 87
<i>Enterococcus spp.</i>	37, 52
<i>Marine bacteria Alteromonas alvinellae</i> and <i>Photobacterium phosphoreum</i>	43
Viruses	
<i>Hepatitis B</i>	44
<i>Bacteriophage MS-2</i>	46, 47
Fungi	
<i>Fusarium spp.</i>	48, 49, 50
<i>Pichia pastoris</i>	51
<i>Candida albicans</i>	52
<i>Aspergillus niger</i>	52
Protozoa	
<i>Giardia intestinalis</i>	53
<i>Acanthamoeba castellani</i>	53
<i>Cryptosporidium parvum</i>	54,55

Table 2

Metabolite	References
Domoic acid	127
Brevotoxin	129
Shellfish toxin – saxitoxin	130
Microcystin	101-120
Nodularin	122
Cylindrospermopsin	123
Anabena	124
Geosmin	125-127
2-methylisoborneol(MIB)	125,128