New Method for the Estimation of Viscosity of Pure and Mixtures of Ionic Liquids Based on the UNIFAC–VISCO Model


Published in:
Journal of Chemical and Engineering Data

Document Version:
Publisher's PDF, also known as Version of record

Queen's University Belfast - Research Portal:
Link to publication record in Queen's University Belfast Research Portal

Publisher rights
Copyright the Authors 2016. This is an open access article published under a Creative Commons Attribution (CC-BY) License, which permits unrestricted use, distribution and reproduction in any medium, provided the author and source are cited.

General rights
Copyright for the publications made accessible via the Queen's University Belfast Research Portal is retained by the author(s) and / or other copyright owners and it is a condition of accessing these publications that users recognise and abide by the legal requirements associated with these rights.

Take down policy
The Research Portal is Queen's institutional repository that provides access to Queen's research output. Every effort has been made to ensure that content in the Research Portal does not infringe any person’s rights, or applicable UK laws. If you discover content in the Research Portal that you believe breaches copyright or violates any law, please contact openaccess@qub.ac.uk.

Open Access
This research has been made openly available by Queen's academics and its Open Research team. We would love to hear how access to this research benefits you. – Share your feedback with us: http://go.qub.ac.uk/oa-feedback
New Method for the Estimation of Viscosity of Pure and Mixtures of Ionic Liquids Based on the UNIFAC–VISCO Model

Nan Zhao, †Johan Jacquemin,* †Ryan Oozeerally, ‡ and Volkan Degirmenci* †‡

†School of Chemistry and Chemical Engineering, Queen’s University Belfast, Belfast, BT9 5AG, U.K.
‡School of Engineering, University of Warwick, Coventry, CV4 7AL, U.K.

ABSTRACT: A modified UNIFAC–VISCO group contribution method was developed for the correlation and prediction of viscosity of ionic liquids as a function of temperature at 0.1 MPa. In this original approach, cations and anions were regarded as peculiar molecular groups. The significance of this approach comes from the ability to calculate the viscosity of mixtures of ionic liquids as well as pure ionic liquids. Binary interaction parameters for selected cations and anions were determined by fitting the experimental viscosity data available in literature for selected ionic liquids. The temperature dependence of the viscosity of the cations and anions were fitted to a Vogel–Fulcher–Tamman behavior. Binary interaction parameters and VFT type fitting parameters were then used to determine the viscosity of pure and mixtures of ionic liquids with different combinations of cations and anions to ensure the validity of the prediction method. Consequently, the viscosities of binary ionic liquid mixtures were then calculated by using this prediction method. In this work, the viscosity data of pure ionic liquids and of binary mixtures of ionic liquids are successfully calculated from 293.15 K to 363.15 K at 0.1 MPa. All calculated viscosity data showed excellent agreement with experimental data with a relative absolute average deviation lower than 1.7%.

1. INTRODUCTION

Ionic liquids (ILs) with negligible vapor pressure at ambient temperature and pressure have made them potential greener alternatives to current solvents. Recent advances have been focused on developing new ILs for use in chemical synthesis, catalysis, and fuel cells.1 ILs are composed of cations and anions; where the cations are typically bulky, asymmetrical, and organic.2,3 Nevertheless, the corresponding anions can be either organic or inorganic.4 The specific chemical and physical properties exhibited by an IL are determined by its particular cation–anion combination. It is theoretically possible to tailor an IL to possess a certain desired set of physical properties by altering its constituent cation–anion pair,5 which are often referred to as task-specific ILs.5,6

Because of the exceedingly large number of potential cation–anion combinations that can be used to synthesize ILs, searching via trial and error for an IL that exhibits the particular set of properties required for a given application at a given temperature and pressure would be impractical, time-consuming, and expensive.4,8 A generic, reliable, and practical method of finding an IL with specific chemical and physical properties is essential to realize the commercial potential of ILs. A practical approach would be to use correlational and/or predictive models.

Viscosity is one of the most widely investigated physical properties, which is of utmost importance for any application.
twenty-six ionic liquids, compromising nine 1-alkyl-3-methylimidazolium cations and eight anions with a temperature range from 258.15 to 433.15 K at atmospheric pressure; 304 data points were correlated with $R^2$ being 0.9888. Among those, eight data points had deviations higher than 30%. Gardas and Coutinho\textsuperscript{17} developed a group contribution method based on the Orrick-Erbar\textsuperscript{18} model. The optimum values of group parameters of eight anions were obtained by minimizing an objective function. The cation was split into the heterocyclic ring, methylene, and methyl groups. The relative group contributions of heterocyclic rings, methylene, and methyl groups were then calculated. A mean percent deviation (MPD) of 7.7% was yielded with a maximum deviation just under 28% for a database of ca. 500 data points for 29 ILs. Daniel et al.\textsuperscript{19} also used the group contribution method based on the Orrick−Erbar equation\textsuperscript{18} for the estimation of a particular group of ILs, such as the magnetic ionic liquids (MILs). Five points for each IL ([P$_{66614}$][GdCl$_6$], [P$_{66614}$][MnCl$_4$], [P$_{66614}$][FeCl$_4$] and [P$_{66614}$][CoCl$_4$]) were used with a result of 7.64% of MPD. It has been reported that Eyring’s theory\textsuperscript{20} was coupled with other models for the viscosity correlation of binary mixtures containing ILs.\textsuperscript{21−23} Wang et al.\textsuperscript{21} calculated the viscosity of ILs with cosolvent mixtures using the Eyring−NRTL and Eyring−UNIQUAC equations. The results for 1014 data points of 35

table: Table 1. Selected Ions, ILs, and References from Which Experimental Data Were Collected

<table>
<thead>
<tr>
<th>anion</th>
<th>Cation</th>
<th>[C$_{1mim}$]$^+$</th>
<th>[C$_{2mim}$]$^+$</th>
<th>[C$_{3mim}$]$^+$</th>
<th>[C$_{4mim}$]$^+$</th>
<th>[C$_{6mim}$]$^+$</th>
<th>[C$_{10mim}$]$^+$</th>
<th>[C$_{4mmim}$]$^+$</th>
<th>[C$_{4py}$]$^+$</th>
<th>[C$_{4m(3)py}$]$^+$</th>
<th>[P$_{66614}$]$^+$</th>
</tr>
</thead>
<tbody>
<tr>
<td>[BF$_4$]$^-$</td>
<td>26</td>
<td>25</td>
<td>26</td>
<td>27</td>
<td>28</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>[C$_{1SO4}$]$^-$</td>
<td>29</td>
<td>30</td>
<td>31</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>[NTf$_2$]$^-$</td>
<td>33</td>
<td>24</td>
<td>34</td>
<td>35</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>[PF$_6$]$^-$</td>
<td>40</td>
<td>41</td>
<td>26</td>
<td>26</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Table 2. Ionic Liquids, Their Corresponding Purities, and Experimental Details for Data Collection Reported in Each Reference

<table>
<thead>
<tr>
<th>Ionic liquid</th>
<th>MW (g/mol)</th>
<th>Temp. range (K)</th>
<th>no. of data points</th>
<th>equipment</th>
<th>purity (wt %)</th>
<th>water content (ppm)</th>
<th>halide content (ppm)</th>
<th>ref</th>
</tr>
</thead>
<tbody>
<tr>
<td>[C$<em>{1mim}$][C$</em>{1SO4}$]</td>
<td>208.24</td>
<td>293.15−343.15</td>
<td>6</td>
<td>capillary tube</td>
<td>NA</td>
<td>&lt;300</td>
<td>NA</td>
<td>29</td>
</tr>
<tr>
<td>[C$_{1mim}$][NTf$_2$]</td>
<td>377.28</td>
<td>298.15−343.15</td>
<td>6</td>
<td>cone−plate viscometer</td>
<td>NA</td>
<td>&lt;10</td>
<td>NA</td>
<td>31</td>
</tr>
<tr>
<td>[C$_{2mim}$][BF$_4$]</td>
<td>197.97</td>
<td>293.15−343.15</td>
<td>7</td>
<td>capillary tube</td>
<td>NA</td>
<td>&lt;30</td>
<td>&lt;30</td>
<td>24</td>
</tr>
<tr>
<td>[C$<em>{2mim}$][C$</em>{1SO4}$]</td>
<td>222.26</td>
<td>293.15−343.15</td>
<td>7</td>
<td>capillary tube</td>
<td>99</td>
<td>&lt;100</td>
<td>NA</td>
<td>30</td>
</tr>
<tr>
<td>[C$_{2mim}$][NTf$_2$]</td>
<td>391.31</td>
<td>293.15−343.15</td>
<td>6</td>
<td>capillary tube</td>
<td>NA</td>
<td>&lt;30</td>
<td>&lt;30</td>
<td>24</td>
</tr>
<tr>
<td>[C$_{3mim}$][BF$_4$]</td>
<td>405.34</td>
<td>318.15−343.15</td>
<td>5</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>50</td>
<td>53</td>
<td>34</td>
</tr>
<tr>
<td>[C$<em>{3mim}$][C$</em>{1SO4}$]</td>
<td>270.16</td>
<td>318.15−343.15</td>
<td>5</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>78.75</td>
<td>&lt;100</td>
<td>40</td>
</tr>
<tr>
<td>[C$_{3mim}$][NTf$_2$]</td>
<td>226.02</td>
<td>293.15−343.15</td>
<td>7</td>
<td>concentric cylinders viscometer</td>
<td>&gt;99.8</td>
<td>146</td>
<td>NA</td>
<td>25</td>
</tr>
<tr>
<td>[C$<em>{4mim}$][C$</em>{1SO4}$]</td>
<td>250.32</td>
<td>293.15−343.15</td>
<td>7</td>
<td>capillary tube</td>
<td>NA</td>
<td>&lt;300</td>
<td>NA</td>
<td>31</td>
</tr>
<tr>
<td>[C$_{4mim}$][NTf$_2$]</td>
<td>419.36</td>
<td>318.15−343.15</td>
<td>5</td>
<td>concentric cylinders viscometer</td>
<td>99</td>
<td>1156</td>
<td>NA</td>
<td>35</td>
</tr>
<tr>
<td>[C$_{4mim}$][PF$_6$]</td>
<td>284.18</td>
<td>318.15−343.15</td>
<td>5</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>&lt;100</td>
<td>NA</td>
<td>41</td>
</tr>
<tr>
<td>[C$_{4mim}$][BF$_4$]</td>
<td>256.08</td>
<td>313.15−363.15</td>
<td>6</td>
<td>cone−plate viscometer</td>
<td>NA</td>
<td>NA</td>
<td>NA</td>
<td>26</td>
</tr>
<tr>
<td>[C$_{4mim}$][PF$_6$]</td>
<td>312.24</td>
<td>313.15−363.15</td>
<td>6</td>
<td>cone−plate viscometer</td>
<td>NA</td>
<td>NA</td>
<td>NA</td>
<td>26</td>
</tr>
<tr>
<td>[C$_{4mim}$][BF$_4$]</td>
<td>310.18</td>
<td>313.15−363.15</td>
<td>6</td>
<td>cone−plate viscometer</td>
<td>NA</td>
<td>NA</td>
<td>NA</td>
<td>26</td>
</tr>
<tr>
<td>[C$_{4mim}$][PF$_6$]</td>
<td>368.34</td>
<td>313.15−363.15</td>
<td>6</td>
<td>cone−plate viscometer</td>
<td>NA</td>
<td>NA</td>
<td>NA</td>
<td>26</td>
</tr>
<tr>
<td>[C$_{4mim}$][BF$_4$]</td>
<td>240.05</td>
<td>298.15−353.15</td>
<td>7</td>
<td>falling/rolling ball viscometer</td>
<td>&gt;99.8</td>
<td>1156</td>
<td>NA</td>
<td>27</td>
</tr>
<tr>
<td>[C$<em>{5mim}$][C$</em>{1SO4}$]</td>
<td>433.39</td>
<td>298.15−353.15</td>
<td>7</td>
<td>concentric cylinders viscometer</td>
<td>&gt;98</td>
<td>24</td>
<td>NA</td>
<td>36</td>
</tr>
<tr>
<td>[C$_{5mim}$][NTf$_2$]</td>
<td>223.02</td>
<td>298.15−353.15</td>
<td>7</td>
<td>falling/rolling ball viscometer</td>
<td>NA</td>
<td>625</td>
<td>&lt;100</td>
<td>28</td>
</tr>
<tr>
<td>[C$<em>{6mim}$][C$</em>{1SO4}$]</td>
<td>416.36</td>
<td>298.15−353.15</td>
<td>7</td>
<td>concentric cylinders viscometer</td>
<td>&gt;99</td>
<td>&lt;100</td>
<td>&lt;100</td>
<td>37</td>
</tr>
<tr>
<td>[C$_{6mim}$][NTf$_2$]</td>
<td>430.39</td>
<td>298.15−353.15</td>
<td>7</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>&lt;100</td>
<td>&lt;100</td>
<td>37</td>
</tr>
<tr>
<td>[C$_{6mim}$][BF$_4$]</td>
<td>216.28</td>
<td>298.15−353.15</td>
<td>6</td>
<td>capillary tube</td>
<td>NA</td>
<td>&lt;730</td>
<td>&lt;1000</td>
<td>42</td>
</tr>
<tr>
<td>[C$<em>{6mim}$][C$</em>{1SO4}$]</td>
<td>253.36</td>
<td>298.15−353.15</td>
<td>6</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>&lt;600</td>
<td>NA</td>
<td>32</td>
</tr>
<tr>
<td>[C$_{6mim}$][NTf$_2$]</td>
<td>422.41</td>
<td>298.15−353.15</td>
<td>6</td>
<td>capillary tube</td>
<td>&gt;99.9</td>
<td>3.6</td>
<td>&lt;1</td>
<td>38</td>
</tr>
<tr>
<td>[C$_{6mim}$][BF$_4$]</td>
<td>764.00</td>
<td>298.15−353.15</td>
<td>6</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>33.6</td>
<td>NA</td>
<td>39</td>
</tr>
<tr>
<td>[P$_{66614}$][NTf$_2$]</td>
<td>549.90</td>
<td>298.15−353.15</td>
<td>6</td>
<td>capillary tube</td>
<td>&gt;99</td>
<td>151</td>
<td>NA</td>
<td>39</td>
</tr>
</tbody>
</table>

MW, molecular weight; NA, not available.
binary systems have been compared. Eyring−UNIQUAC gave a better accuracy with the RAAD being 2.61% than the Eyring−NRTL equation (3.5%). He et al.23 performed three methods (Eyring−Wilson, Eyring−NRTL and Eyring−UNIQUAC) for the correlation of binary mixtures with ILs by collecting 1560 data points of 49 mixtures. The results showed that the Eyring−Wilson equation gave almost the same accuracy as the Eyring−UNIQUAC equation and a better performance than the Eyring−NRTL equation. The Eyring−Wilson equation has a more simple mathematical form than the Eyring energy parameters within the IL mixture.

The Eyring−Wilson equation was used in any other mixture of ILs which happens to have same anion−cation combination. But experimental data is needed to estimate the viscosity of pure or mixed ionic liquids. In our original approach, the anion and cation of each IL are considered as individual groups. A set of experimental data available in the literature was used to determine the UNIFAC−VISCO model parameters for each anion and cation. Successively, ILs were constructed by different combinations of cations and anions and their viscosities were determined. This method was then extended for the determination of the viscosity of binary mixtures of ILs as the function of the composition and temperature at 0.1 MPa. Similarly, the anions and cations within the mixture were treated as individual groups.

The new method proposed herein is applicable to any family of ILs; any cation/anion structure and combination. Therefore, it is a generic method. The VFT parameters obtained for one cation (or anion) from one IL can be used for the prediction of viscosity of any other ILs or ILs mixture containing the same cation (or anion). The group interaction potential energy parameters calculated by fitting the viscosity of one IL can be used in any other mixture of ILs which happens to have same anion−cation combination. But experimental data is needed to determine any remaining unknown group interaction potential energy parameters within the IL mixture.

In this paper, we report the successful development of this method for the prediction of viscosity of pure ILs and their mixtures as the function of the IL structure, composition, and temperature at 0.1 MPa.

2. DATA COLLECTION

To develop the UNIFAC−VISCO-based model for ILs, 25 different ILs from 19 different references (154 data points) were chosen.24−42 The selected ILs are among the most commonly studied with a large number of experimentally available viscosity data in the literature. This work is a proof of concept study to demonstrate the potential of the proposed method for the prediction of the viscosity of ILs. Therefore, a limited number of ILs were used by carefully selecting the data from the available literature depending on the purity, viscosity measurement method, and temperature.

The cations used are imidazolium, pyridinium, pyrrolidinium, and phosphonium-based structures. Five different inorganic anions are used, for example, bis(trifluoromethylsulfonyl)imide ([NTf2]−), hexafluorophosphate ([PF6]−), and dicyanamide ([DCA]−). Selected cations and anions are listed in Table 1 along with the references from which the experimental viscosity data were taken. The temperature range, number of data points in each reference, molecular weight, purity of ionic liquids, contents of impurity, and measurement methods are summarized in Table 2.

The accuracy of the viscosity measurements strongly depends on the purity of the ionic liquid used. The most common impurities found within ILs include water, halides (chloride, bromide, iodide), metals (lithium, sodium, etc.), and unreacted reagents.53 Specifically chloride and water have a dramatic effect on the viscosity of ILs. Typically the presence of chloride increases generally the viscosity of the IL. Conversely water decreases (generally) the ILs viscosity.44 In a comparison of the IL [C4mim][BF4] reported by Nikitina et al.45 and by Vakili et al.25 up to a 1% difference in its viscosity is observed especially at lower temperatures (see Figure S1 of the Electronic Supporting Information, ESI). Therein, the water content of [C4mim][BF4] was reported to be below 15 ppm in the former study and an order of magnitude higher (146 ppm) in the latter study. Therefore, the viscosity values taken from Vakili et al.25 are smaller than those from Nikitina et al.45 at any same temperature, due to the increased concentration of water. Similarly, the effects of different batches of a common IL on the viscosity can be seen by comparing the viscosity data of [C4py][BF4] samples (Figure S2 of ESI). Larriba et al.46 purchased [C4py][BF4] samples from Iolitec GmbH with a water level lower than 100 ppm and chloride content less than 100 ppm. While Mokhtari et al.28 synthesized [C4py][BF4] in their own laboratory with water content of 625 ppm and bromide content less than 100 ppm. The viscosities of these two samples were both determined with an Anton Paar automated microviscometer (AMVn).

The viscosity measurement techniques are another source of deviation in the accuracy of viscosity data in literature. García-Mardones et al.57 also obtained [C4py][BF4] from Iolitec; however, García-Mardones et al.45 used a set of Ubbelohde viscometers to measure the viscosity of [C4py][BF4]. At 293.15 K, the value measured by Larriba et al.46 (227.1 mPa·s) is 1.7% higher than the viscosity measured by Mokhtari et al.28 and 2.8% higher than the viscosity measured by García-Mardones et al.57 This clearly shows that in some cases the experimental techniques have an even more dramatic effect on the measured viscosities than the water content when the IL is dried under vacuum prior to its use.

Discrepancies in the experimental data affect the quality of the correlation and thus the development of the predictive method. Therefore, in this study, we have only selected experimental data with the lowest halide and water impurity. As a proof of concept study, we selected data with low levels of impurities in order to reduce errors. The quantity of water, halide, and impurity levels are given in Table 2. In addition, to eliminate the negative effect of systematic errors for the development of our new method, we used only one data set from a single reference for each IL to develop the proposed UNIFAC−VISCO-based model.

3. DEVELOPMENT OF THE UNIFAC−VISCO METHOD FOR IONIC LIQUIDS

3.1. Calculation of the Viscosity by the UNIFAC−VISCO Method. The UNIFAC−VISCO model is a group
contribution model developed by Chevalier et al.\textsuperscript{48,49} to predict the viscosities of liquid mixtures. This model is based on the theory of Eyring and the UNIFAC group contribution model proposed originally by Fredenslund et al.\textsuperscript{50}

The viscosity calculation (eq 1) by using UNIFAC–VISCO method is described as follows:\textsuperscript{48,49,51}

\[
\ln(\mu) = \sum_{i=1}^{C} x_i \ln \left( \frac{V_i}{V_m} \right) + \frac{g^{E}_c}{RT} - \frac{g^{E}_r}{RT} \tag{1}
\]

where \( \mu \) is the mixtures viscosity (mPa⋅s); subscript \( i \) represents the component; \( C \) is the total number of components; \( x_i \) is the mole fraction of the component \( i \). \( V_i \) is the molar volume (m\(^3\)/kmol) of the pure component \( i \), while \( V_m \) is molar volume (m\(^3\)/kmol) of the mixture. \( R \) is the gas constant (J/mol⋅K) and \( T \) is temperature (K). \( g^c \) and \( g^r \) are the combinatorial and the residual contribution terms of the UNIFAC–VISCO method, respectively.

The combinatorial contribution term (eq 2) is defined as

\[
g^c = \sum_{i} x_i \ln \frac{\phi_i}{x_i} + \frac{z}{2} \sum_{i} x_i q_i \ln \frac{\theta_i}{\phi_i} \tag{2}
\]

where \( z \) is a coordinate value equal to 10 and \( x_i \) is the mole fraction of the component \( i \). \( \phi_i \) is the molecular volume fraction of component \( i \); \( q_i \) represents the van der Waals’ surface area of component \( i \); and \( \theta_i \) is the molecular surface area fraction of component \( i \).

\( \theta_i \) and \( \phi_i \) can be obtained by the following eqs 3 and 4:

\[
\theta_i = \frac{x_i q_i}{\sum x_j q_j} \tag{3}
\]

\[
\phi_i = \frac{x_i \theta_i}{\sum x_j \theta_j} \tag{4}
\]

where subscript \( i \) and \( j \) represent the components, \( q_i \) and \( q_j \) represent the van der Waals’ surface area of components \( i \) and \( j \), respectively, and \( r_i \) and \( r_j \) represent the van der Waals’ volume of components \( i \) and \( j \), respectively.

The surface area \( (q) \) and the volume \( (r) \) can be determined by the following eqs 5 and 6:

\[
q_i = \sum_{k=1}^{N} n_{i,k} Q_k \tag{5}
\]

\[
r_i = \sum_{k=1}^{N} n_{i,k} R_k \tag{6}
\]

where subscript \( k \) denotes the groups; \( n_{i,k} \) is the total number of \( k \)th group present in component \( i \); \( N \) is the total number of groups present; \( Q_k \) is the group surface area parameter; and \( R_k \) is the group volume parameter.

The residual contribution (eq 7) term is defined as

\[
g^r = \sum_{i=1}^{C} x_i \sum_{m=1}^{N} n_{m,i} \left( \ln \gamma_m - \ln \gamma_{m,i} \right) \tag{7}
\]

where \( C \) is the total number of components; \( x_i \) is the fraction of component \( i \) in the mixture; \( N \) is the total number of groups; \( n_{m,i} \) and \( \gamma_m \) refer to the group values in the mixture, and \( n_{m,i} \) and \( \gamma_{m,i} \) refer to the group values in pure-component.

In \( \gamma_m \) represents the residual activity coefficient and can be obtained by using eq 8:

\[
\ln \gamma_m = Q_m \left[ 1 - \ln \left( \sum_{i=1}^{N} \Theta_i \Psi_{m,i} \right) - \sum_{i=1}^{N} \frac{\Theta_i \Psi_{m,i}}{\sum_{j=1}^{N} \Theta_j \Psi_{j,i}} \right] \tag{8}
\]

where \( N \) is the total number of groups present; \( \Theta_i \) represents the surface area fraction for group \( i \); and \( \Psi_{m,i} \) represents the group interaction parameters.

The \( \Theta \) values for each group both in mixture and in pure component can be calculated using eq 9:

\[
\Theta_m = \frac{x_m Q_m}{\sum_{i=1}^{N} x_i Q_i}, \quad m = 1, 2, 3...N \tag{9}
\]

where the subscripts represent the groups.

The group interaction parameters \( (\Psi) \) are then calculated by using eq 10:

\[
\Psi_{mn} = \exp \left( -\frac{\alpha_{mn}}{298.15} \right) \tag{10}
\]

where \( \alpha_{mn} \) are group interaction potential energy parameters between the groups \( m \) and \( n \). It is important to note that the values for the group interaction parameters \( \alpha_{mn} \) and \( \alpha_{nm} \) are not the same.

3.2. Calculation of Ionic Liquid Viscosity by the UNIFAC–VISCO Method. The viscosity of the pure ILs is calculated by the UNIFAC–VISCO method by following an original approach, in which the cation and anion, constituting each ionic liquid, are regarded as individual groups. In this case, each component is made up of a single group (either cation or anion). Sample calculations for a pure IL and a binary mixture of ILs by using our model based on the UNIFAC–VISCO method are given in the Supporting Information.

The first set of parameters required for the calculation of IL viscosity using the UNIFAC–VISCO method is the molar volume \( (V) \) of pure components and the molar volume of their mixture \( (V_m) \). For a single ionic liquid, these correspond to the effective molar volume of the cation and anion (i.e., components) and the molar volume of pure ionic liquid, respectively. It is not straightforward to obtain the effective molar volumes of ions. However, in our previous study,\textsuperscript{43,52} we developed a group contribution model to predict the volumetric properties of ILs.

In this case, the mixture of anion and cation is considered to be ideal.\textsuperscript{43,52} The quadratic eq 11 was used to fit the experimental volumetric data as a function of temperature at a reference pressure (0.1 MPa).

\[
V_m(T, P_{ref}) = \sum_{i=0}^{2} \left( b_i(T) P_{ref} \right) \tag{11}
\]

where \( P_{ref} = 0.1 \) MPa and \( b_i \) is the fitting parameters.

The Jacquemin et al.\textsuperscript{43,52} method has been further extended to calculate the effective molar volumes of individual cations and anions. Fitting parameters for the calculation of the effective molar volumes of selected ions at 0.1 MPa used in this study are given in Table S1 of the Supporting Information. The effective molar volumes of the cations \( (V^c) \) and anions \( (V^a) \) can be calculated as a function of temperature and pressure by following eq 11 and eq 12.

\[
V_m(T^*, P_{ref}) = V^c_m(T^*, P_{ref}) + V^a_m(T^*, P_{ref}) \tag{12}
\]
where \( T^* = T - 298.15 \), \( p_{ref} = 0.1 \text{ MPa} \), and \( a_i \) is the effective molar volume group contribution parameter as described by Jacquemin et al.\(^{35,32}\).

The second set of parameters required for the calculation of IL viscosities using the UNIFAC–VISCO method is the cations and anions volume \( R \) and surface area \( Q \) parameters. The \( R \) and \( Q \) values of cations and anions used in this study were obtained using COSMOTherm software (version C30_1501) following the methodology previously described by our group\(^{35}\) and are given in Table S2 of the Supporting Information.

In the UNIFAC–VISCO method, individual component viscosities, that is, the effective viscosity of each ion, are required (see eq 1). Furthermore, in this work, the temperature dependence on the effective viscosity of each ion, \( \mu_{ion} \), is represented by the Vogel–Fulcher–Tamman (VFT) type fitting equation:

\[
\mu_{ion} = A \exp \left( \frac{B}{T - T_0} \right)
\]

(14)

where \( A \), \( B \), and \( T_0 \) are the fitting parameters of the effective viscosity of each ion.

Another set of parameters required in the UNIFAC–VISCO method are the mole fractions of components. In our approach we assumed that the components, i.e., the cations and anions, contribute equally to the viscosity of the pure ionic liquid or the mixture of ionic liquids. Therefore, in the calculation of the viscosity of pure ionic liquids, the mole fractions of ions were taken as equal to 0.5. Similarly, in the calculation of binary mixtures of ionic liquids, the mole fraction of each ion is taken as equal to 0.25.

The viscosity data were then correlated by minimizing the objective function (eq 15) using the Marquardt\(^{34}\) optimization technique to estimate the unknown parameters of the UNIFAC–VISCO group interaction potential energy parameters and VFT fitting parameters:

\[
OF = \frac{1}{M} \sum_{j=1}^{M} \left( \frac{\mu_{exp} - \mu_{calc}}{\mu_{exp}} \right)^2 \rightarrow \text{min}
\]

(15)

where \( M \) is the number of data points; \( \mu_{exp} \) and \( \mu_{calc} \) are the experimental and calculated viscosity data, respectively.

For each ionic liquid, eight parameters are required for the calculation of viscosity by the UNIFAC–VISCO method. These parameters are the group interaction potential energy parameters of cation and anion \( (a_{mol}, a_{ion}) \) and the VFT fitting parameters for each cation and anion defining the temperature dependency of viscosity \( (A, B, T_0) \) for each cation and anion. During this work, the Solver tool in Microsoft Excel was used to obtain initial estimates for required parameters. These parameters were then used as initial guess values in a MATLAB script, which was developed to achieve the calculation process by using a nonlinear least-squares regression method.

The accuracy of the fitting parameters depends on the available number of experimental data points. On the basis of our approach, the VFT parameters and group interaction potential energy parameters are cation and anion specific and thus must be the same irrespective of the IL structure. Therefore, performing the regression analysis of ionic liquids with common cations and anions decreases the number of unknown parameters relative to the available experimental data. Herein, first we used four ILs with common ions for calculations accordingly. An example of this approach is shown in Scheme 1.

### Scheme 1. Example of the Methodology Used during the Regression Analysis

<table>
<thead>
<tr>
<th>Ionic Liquid</th>
<th>Cation</th>
<th>Anion</th>
</tr>
</thead>
<tbody>
<tr>
<td>[C(_2)mim](^+)</td>
<td>[BF(_4)](^-)</td>
<td></td>
</tr>
<tr>
<td>[C(_4)mim](^+)</td>
<td>[BF(_4)](^-)</td>
<td></td>
</tr>
<tr>
<td>[C(_4)mim](^+)</td>
<td>[NTf(_2)](^-)</td>
<td></td>
</tr>
<tr>
<td>[C(_2)mim](^+)</td>
<td>[NTf(_2)](^-)</td>
<td></td>
</tr>
</tbody>
</table>

For example, the following four ionic liquids; [C\(_2\)mim][BF\(_4\)], [C\(_4\)mim][BF\(_4\)], [C\(_4\)mim][NTf\(_2\)]\(^-\), and [C\(_2\)mim][NTf\(_2\)]\(^-\) are based on two different cations ([C\(_4\)mim]\(^+\) and [C\(_2\)mim]\(^+\)]) and two different anions ([BF\(_4\)]\(^-\) and [NTf\(_2\)]\(^-\)). A total of 20 unknown parameters, that is, two group interaction potential energy parameters for each IL and three sets of VFT parameters for each individual ion, were calculated by regression analysis. This is a significant reduction in the number of parameters required and consequently the number of initial guess values in order to correlate UNIFAC–VISCO based model. Since VFT parameters do not depend on temperature, more experimental data at different temperatures improve the quality of the fit, because the number of fitting parameters relative to the available experimental data decreases significantly.

Sample viscosity calculations for pure ILs and binary mixture of ILs and MATLAB files are provided in the Supporting Information. First MATLAB program (Filename: IonicLiquidViscosityCalculator) contains all parameters (binary interaction and VFT parameters) estimated during this study. This program can be used to determine the viscosity of selected ionic liquids and it could be further extended to include additional ILs. Another set of MATLAB program files (PureILs and BinaryILs) were developed for the estimation of UNIFAC–VISCO parameters by the built-in functions of least-square method.

### 4. RESULTS AND DISCUSSION

Group interaction potential energy and VFT parameters were estimated by following the regression analysis (eq 15) of the experimental data for selected pure ILs (see Tables 1 and 2). The calculated binary group interaction potential energy parameters \( (a_{mol}, a_{ion}) \) for the cation and anion pairs are given in Table 3, while the VFT parameters of selected cations and anions are given in Table 4.
The quality of the regression was then determined by calculating the relative absolute average deviations (RAAD, eq 16) between the calculated and the experimental viscosity data.

$$\text{RAAD} = 100 \times \frac{1}{M} \sum_{i} \left| \frac{\mu_{\text{exp}} - \mu_{\text{cal}}}{\mu_{\text{exp}}} \right|$$

The RAAD values for the regression of pure ILs and binary mixtures of ILs are reported in Tables 5 and 6, respectively. For the regression of the pure ILs, it appears that the RAADs are lower than 1% for all the investigated ILs except in the case of \([\text{[C10mim]}][\text{BF}_4] \) (RAAD = 1.61%) and \([\text{[C4py]}][\text{BF}_4] \) (RAAD = 1.25%). This shows that the regression of the viscosity data of pure ILs using the UNIFAC–VISCO method is achieved with accuracy better than 1.7% with the respect of the selected experimental data. For the calculation of the relative average absolute deviation, 1.7%, all the experimental data were used. This is the accuracy obtained by using the carefully selected data to develop the model. Therefore, the reported accuracy of 1.7% represents the correlation ability of the model.

The comparison of experimental and calculated viscosity data with our model is shown in Figure 1 in the case of the pure ILs investigated during this work (see Tables 1 and 2). A good agreement between the UNIFAC–VISCO model and the experimental data is observed (see Figure 1 and Figure S3 of the Supporting Information).

A limited number of viscosity data for binary mixtures of ionic liquids has been reported in the literature to date. By using the group interaction potential energy and VFT parameters obtained by the regression of the pure ILs and by following the same methodology, the viscosity of binary mixtures of ILs were then correlated by the UNIFAC–VISCO model. The viscosity data of four binary mixtures of ILs reported in the literature,55 were used to exemplify the feasibility to extend our approach in the case of the mixture of two pure ILs. The compositions of the mixtures, temperature range, and number of data reported by Navia et al.55 are summarized in Table 6. Herein one set of data for each binary mixture was correlated for the group interaction potential energy parameters (see Table 7). The other data of each mixture were used to compare with the predicted viscosities.

### Table 4. VFT Fitting Parameters of the Selected Cations and Anions

<table>
<thead>
<tr>
<th>cation/anion</th>
<th>A (mPa·s)</th>
<th>B (K)</th>
<th>T₀ (K)</th>
</tr>
</thead>
<tbody>
<tr>
<td>([\text{[C2mim]}]^+)</td>
<td>0.1242</td>
<td>963.7</td>
<td>122.1</td>
</tr>
<tr>
<td>([\text{[C4mim]}]^+)</td>
<td>0.0617</td>
<td>981.2</td>
<td>155.5</td>
</tr>
<tr>
<td>([\text{[C3mim]}]^+)</td>
<td>0.2703</td>
<td>501.9</td>
<td>191.9</td>
</tr>
<tr>
<td>([\text{[C4m(3)py]}]^+)</td>
<td>0.2641</td>
<td>791.9</td>
<td>186.7</td>
</tr>
<tr>
<td>([\text{[P66614]}]^+)</td>
<td>5.2975</td>
<td>658.2</td>
<td>172.4</td>
</tr>
<tr>
<td>([\text{[C2mim]}][\text{BF}_4] )</td>
<td>0.1219</td>
<td>865.0</td>
<td>199.0</td>
</tr>
<tr>
<td>([\text{[C4py]}]^+)</td>
<td>0.0353</td>
<td>710.7</td>
<td>187.6</td>
</tr>
<tr>
<td>([\text{[C4py]}]^+)</td>
<td>0.0065</td>
<td>1639</td>
<td>124.2</td>
</tr>
<tr>
<td>([\text{[C4py]}]^+)</td>
<td>0.0091</td>
<td>1671</td>
<td>121</td>
</tr>
<tr>
<td>([\text{[C1mim]}]^+)</td>
<td>0.6941</td>
<td>330.0</td>
<td>204.5</td>
</tr>
<tr>
<td>([\text{[C4mpyrr]}]^+)</td>
<td>0.0469</td>
<td>932.7</td>
<td>178.9</td>
</tr>
<tr>
<td>([\text{[BF}_4]^-)</td>
<td>3.7391</td>
<td>352.1</td>
<td>204.2</td>
</tr>
<tr>
<td>([\text{[C1SO_4]}^-)</td>
<td>0.8313</td>
<td>675.3</td>
<td>186.5</td>
</tr>
<tr>
<td>([\text{[NTf}_2^-)</td>
<td>1.2222</td>
<td>548.7</td>
<td>125.3</td>
</tr>
<tr>
<td>([\text{[PF}_6^-)</td>
<td>3.2320</td>
<td>370.2</td>
<td>219.4</td>
</tr>
<tr>
<td>([\text{[DCA]}^-)</td>
<td>2.6871</td>
<td>370.5</td>
<td>118.1</td>
</tr>
</tbody>
</table>

The quality of the regression was then determined by calculating the relative absolute average deviations (RAAD, eq 16) between the calculated and the experimental viscosity data.
The prediction result is highlighted by the RAAD values, reported in Table 8, which is 5% for all reported binary data published by Navia et al.55

In addition the parity plot given in Figure 2 shows good agreement between the experimental data and calculated viscosity values by using the UNIFAC−VISCO model with the exception of a visual larger deviation at higher mole fraction of [C4mim][PF6] in the binary system ([C4mim][PF6] and [C4mim][BF4]). This good agreement is also attested by the calculated relative deviations between the experimental and predicted viscosity data for selected binary ILs as shown in Figure S4 of the Supporting Information.

5. CONCLUSIONS
An original method for the determination of the viscosity of ionic liquids and mixtures of ionic liquids was developed. The model is based on the UNIFAC−VISCO model in which the cations and anions constituting the ionic liquids are regarded as individual components. The regression analysis was performed with single ionic liquids to estimate the group interaction potential energy and VFT parameters of each ion. The RAAD is below 1.7% for all ionic liquids studied. The viscosity of binary mixtures of ionic liquids was then calculated and Table 7. Selected sets of binary mixtures of ILs. Experimental data were taken from Navia et al.55 for regression

![Graph](image1.png)

**Figure 1.** Comparison of experimental viscosity and predicted viscosity for pure ionic liquids.

![Graph](image2.png)

**Figure 2.** Comparison of experimental viscosity and predicted viscosity for binary ionic liquids where data used for developing correlation (●) and predicted data (○) are shown.

<table>
<thead>
<tr>
<th>binary system</th>
<th>mole fraction range (x)</th>
<th>temp range (K)</th>
<th>no. of data points</th>
</tr>
</thead>
<tbody>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C2mim][BF4]</td>
<td>0.0978−0.9455</td>
<td>298.15−308.15</td>
<td>9</td>
</tr>
<tr>
<td>x[C4mim][BF4] + (1 − x)[C4mim][C1SO4]</td>
<td>0.1209−0.9447</td>
<td>298.15−308.15</td>
<td>9</td>
</tr>
<tr>
<td>x[C4mim][PF6] + (1 − x)[C4mim][BF4]</td>
<td>0.0568−0.945</td>
<td>298.15−308.15</td>
<td>9</td>
</tr>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C4mim][BF4]</td>
<td>0.1083−0.946</td>
<td>298.15−308.15</td>
<td>9</td>
</tr>
</tbody>
</table>

Table 6. Binary Viscosity Data Adapted from Navia et al.55

<table>
<thead>
<tr>
<th>binary system</th>
<th>mole fraction range (x)</th>
<th>temp range (K)</th>
<th>no. of data points</th>
</tr>
</thead>
<tbody>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C2mim][BF4]</td>
<td>0.0978−0.9455</td>
<td>298.15−308.15</td>
<td>117</td>
</tr>
<tr>
<td>x[C4mim][BF4] + (1 − x)[C4mim][C1SO4]</td>
<td>0.1209−0.9447</td>
<td>298.15−308.15</td>
<td>117</td>
</tr>
<tr>
<td>x[C4mim][PF6] + (1 − x)[C4mim][BF4]</td>
<td>0.0568−0.945</td>
<td>298.15−308.15</td>
<td>99</td>
</tr>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C4mim][BF4]</td>
<td>0.1083−0.946</td>
<td>298.15−308.15</td>
<td>9</td>
</tr>
</tbody>
</table>

Table 7. Relative Absolute Average Deviation (RAAD) of the Calculated Viscosity from the Experimental Viscosity Data for Selected ILs

<table>
<thead>
<tr>
<th>ionic liquid</th>
<th>RAAD (%)</th>
<th>ionic liquid</th>
<th>RAAD (%)</th>
<th>ionic liquid</th>
<th>RAAD (%)</th>
<th>ionic liquid</th>
<th>RAAD (%)</th>
<th>ionic liquid</th>
<th>RAAD (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>[C1mim][C1SO4]</td>
<td>0.49</td>
<td>[C3mim][NTf2]</td>
<td>0.19</td>
<td>[C4mim][PF6]</td>
<td>1.02</td>
<td>[C4mmim][BF4]</td>
<td>0.33</td>
<td>[C4m(3)py][DCA]</td>
<td>0.75</td>
</tr>
<tr>
<td>[C1mim][NTf2]</td>
<td>0.60</td>
<td>[C3mim][PF6]</td>
<td>0.16</td>
<td>[C4mim][BF4]</td>
<td>0.54</td>
<td>[C4mmim][NTf2]</td>
<td>0.77</td>
<td>[C4m(3)py][NTf2]</td>
<td>1.43</td>
</tr>
<tr>
<td>[C2mim][BF4]</td>
<td>0.20</td>
<td>[C4mim][BF6]</td>
<td>0.37</td>
<td>[C4py][BF4]</td>
<td>0.60</td>
<td>[C4py][NTf2]</td>
<td>1.25</td>
<td>[P66614][NTf2]</td>
<td>0.73</td>
</tr>
<tr>
<td>[C2mim][C1SO4]</td>
<td>0.08</td>
<td>[C4mim][C1SO4]</td>
<td>0.11</td>
<td>[C6mim][BF4]</td>
<td>1.61</td>
<td>[C6mim][NTf2]</td>
<td>0.31</td>
<td>[P66614][DCA]</td>
<td>0.26</td>
</tr>
<tr>
<td>[C2mim][NTf2]</td>
<td>0.58</td>
<td>[C4mim][NTf2]</td>
<td>0.27</td>
<td>[C1mim][C1SO4]</td>
<td>0.08</td>
<td>[C4mim][NTf2]</td>
<td>0.27</td>
<td>[C4mim][BF4]</td>
<td>0.48</td>
</tr>
</tbody>
</table>

Table 8. Relative Absolute Average Deviations (RAAD) of Viscosity Predictions from the Experimental Viscosity Data for Binary Mixtures of ILs

<table>
<thead>
<tr>
<th>binary system</th>
<th>RAAD (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C2mim][BF4]</td>
<td>3.2</td>
</tr>
<tr>
<td>x[C4mim][BF4] + (1 − x)[C4mim][C1SO4]</td>
<td>3.8</td>
</tr>
<tr>
<td>x[C4mim][PF6] + (1 − x)[C4mim][BF4]</td>
<td>3.8</td>
</tr>
<tr>
<td>x[C6mim][BF4] + (1 − x)[C4mim][BF4]</td>
<td>8.2</td>
</tr>
<tr>
<td>all mixtures</td>
<td>5.0</td>
</tr>
</tbody>
</table>
compared with experimental data available in the literature. It turned out that the RAAD is 5% for all mixtures. This shows that the UNIFAC–VISCO model can be used to correlate and predict the viscosities of pure ionic liquids as well as mixtures of ionic liquids with great accuracy.

ASSOCIATED CONTENT

Supporting Information
The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acs.jced.6b00161.

Comparisons of two experimental data sets available in the literature in the case of the \([\text{C}_6\text{mim}]^+\text{BF}_4^-\) and \([\text{C}_4\text{mpy}]\text{BF}_4^-\) are reported in Figures S1–S2, respectively. The relative deviations between the experimental and predicted viscosity data for pure ionic liquids and selected binary mixtures of ILs are reported in Figures S3–S4, respectively. Furthermore, all effective molar volume parameters, \(R\) and \(Q\) values for each ion estimated during this work, are tabulated in Tables S1–S2. Examples of the viscosity calculations for a pure IL and a binary mixture of ILs are given. Component viscosities, component molar volumes, groups, area fractions, volume fractions, group interactions, group fractions required for the viscosity calculation are given in Tables S3–13 (PDF)

AUTHOR INFORMATION

Corresponding Authors
*E-mail: johan.jacquemin@qub.ac.uk.
*E-mail: v.degirmenci@warwick.ac.uk.

Funding
N.Z. and J.J. acknowledge gratefully the CEA le Ripault (Grant No 4600261677/P6E31) and the Engineering and Physical Sciences Research Council (EPSRC) for supporting this work financially (EPSRC First Grant Scheme, Grant No EP/M021785/1).

Notes
The authors declare no competing financial interest.

ABBREVIATIONS

Cations
\[\text{[C}_6\text{mim}]^+\] 1,3-dimethylimidazolium
\[\text{[C}_2\text{mim}]^+\] 1-ethyl-3-methylimidazolium
\[\text{[C}_3\text{mim}]^+\] 1-propyl-3-methylimidazolium
\[\text{[C}_4\text{mim}]^+\] 1-butyl-3-methylimidazolium
\[\text{[C}_6\text{mim}]^+\] 1-hexyl-3-methylimidazolium
\[\text{[C}_{10}\text{mim}]^+\] 1-decyl-3-methylimidazolium
\[\text{[C}_{10m}\text{im}]^+\] 1-butyl-2,3-methylimidazolium
\[\text{[C}_3\text{py}]^+\] 1-butylpyridinium
\[\text{[C}_4\text{m(3)py}]^+\] 1-butyl-3-methylpyridinium
\[\text{[C}_3\text{mpyrr}]^+\] 1-butyl-1-methylpyrrolidinium
\[\text{[P}_{66614}^+]\] trihexyl(tetradecyl)phosphonium

Anions
\[\text{[BF}_4^-\] tetrafluoroborate
\[\text{[NTE}_4^-\] bis(trifluoromethylsulfonyl)amide
\[\text{[GdCl}_4^2-\] gadolinium tetrafluoroborate
\[\text{[MnCl}_4^2-\] tetrachloromanganese
\[\text{[FeCl}_4^2-\] tetrachloroferrate
\[\text{[CoCl}_4^2-\] tetrachlorocobalt
\[\text{[C}_3\text{SO}_4^-\] methysulfate

\[\text{[PF}_6^-\] hexafluorophosphate
\[\text{[DCA]}\] dicyanamide

Nomenclature

Roman Letters
\(a\) Tait equation parameter
\(b\) Tait equation parameter
\(A\) VFT equation parameter
\(B\) VFT equation parameter
\(C\) total number of components in UNIFAC–VISCO method
\(g\) combinatorial contribution term in UNIFAC–VISCO method
\(g'_r\) residual contribution term in UNIFAC–VISCO method
\(n_k\) total number of \(k\)th group present in component \(i\)
\(N\) total number of groups
\(P_{\text{ref}}\) reference pressure (0.1 MPa)
\(q\) van der Waals’ surface area of component \(i\)
\(Q_i\) group surface area parameter
\(r\) van der Waals’ volume of component \(i\)
\(R_i\) group volume parameter
\(R\) gas constant (J/mol-K)
\(T\) temperature (K)
\(T_e\) VFT equation parameter
\(V_i\) pure-component molar volume (m^3/kmol)
\(V_m\) mixture molar volume (m^3/kmol)
\(x_i\) mole fraction of the component \(i\)
\(z\) coordinate value in UNIFAC–VISCO method

Greek Letters
\(\alpha_m\) group interaction potential energy parameter between groups \(m\) and \(n\)
\(\gamma_m\) residual activity coefficient
\(\theta_i\) molecular surface area fraction of component \(i\)
\(\Theta_i\) surface area fraction for group \(i\)
\(\mu\) viscosity of mixture (mPa·s)
\(\mu_i\) viscosity of component \(i\)
\(\mu_{\exp}\) viscosity experimentally measured
\(\mu_{\text{calc}}\) viscosity calculated by our method
\(\rho_a\) density
\(\phi_i\) molecular volume fraction of component \(i\)
\(\psi_{m,n}\) group interaction parameter

REFERENCES

(9) Meindersma, W. G. W.; van Acker, T.; de Haan, A. B. Physical Properties of 3-Methyl-N-Butylpyridinium Tricyanomethanide and
Ternary LLE Data with an Aromatic and an Aliphatic Hydrocarbon at T = (303.2 and 328.2)K and p = 0.1 MPa. Fluid Phase Equilib. 2011, 307, 30–38.


