Biobutanol as Fuel for Direct Alcohol Fuel Cells—Investigation of Sn-Modified Pt Catalyst for Butanol Electro-oxidation

Vinod Kumar Puthiyapura,† Dan J. L. Brett,‡ Andrea E. Russell,§ Wen-Feng Lin,*†∥ and Christopher Hardacre†§,

†Centre for the Theory and Application of Catalysis (CenTACat), School of Chemistry and Chemical Engineering, Queen’s University of Belfast (QUB), Belfast, BT9 5AG, U.K.
‡Department of Chemical Engineering and Analytical Science, The University of Manchester, The Mill, Manchester, M13 9PL, U.K.
§Department of Chemical Engineering, Loughborough University, Loughborough, Leicestershire, LE11 3TU, U.K.
∥Department of Chemical Engineering, University College London (UCL), London WC1E 7JE, U.K.

Supporting Information

ABSTRACT: Direct alcohol fuel cells (DAFCs) mostly use low molecular weight alcohols such as methanol and ethanol as fuels. However, short-chain alcohol molecules have a relative high membrane crossover rate in DAFCs and a low energy density. Long chain alcohols such as butanol have a higher energy density, as well as a lower membrane crossover rate compared to methanol and ethanol. Although a significant number of studies have been dedicated to low molecular weight alcohols in DAFCs, very few studies are available for longer chain alcohols such as butanol. A significant development in the production of biobutanol and its proposed application as an alternative fuel to gasoline in the past decade makes butanol an interesting candidate fuel for fuel cells. Different butanol isomers were compared in this study on various Pt and PtSn bimetallic catalysts for their electro-oxidation activities in acidic media. Clear distinctive behaviors were observed for each of the different butanol isomers using cyclic voltammetry (CV), indicating a difference in activity and the mechanism of oxidation. The voltammograms of both n-butanol and iso-butanol showed similar characteristic features, indicating a similar reaction mechanism, whereas 2-butanol showed completely different features; for example, it did not show any indication of poisoning. Ter-butanol was found to be inactive for oxidation on Pt. In situ FTIR and CV analysis showed that OHads was essential for the oxidation of primary butanol isomers which only forms at high potentials on Pt. In order to enhance the water oxidation and produce OHads at lower potentials, Pt was modified by the oxophilic metal Sn and the bimetallic PtSn was studied for the oxidation of butanol isomers. A significant enhancement in the oxidation of the 1° butanol isomers was observed on addition of Sn to the Pt, resulting in an oxidation peak at a potential ~520 mV lower than that found on pure Pt. The higher activity of PtSn was attributed to the bifunctional mechanism on PtSn catalyst. The positive influence of Sn was also confirmed in the PtSn nanoparticle catalyst prepared by the modification of commercial Pt/C nanoparticle and a higher activity was observed for PtSn (3:1) composition. The temperature-dependent data showed that the activation energy for butanol oxidation reaction over PtSn/C is lower than that over Pt/C.

KEYWORDS: butanol, biobutanol, direct alcohol fuel cells, electrocatalyst, PtSn, bifunctional mechanism

1. INTRODUCTION

Direct alcohol fuel cells (DAFCs) are promising alternative power sources and have advantages over hydrogen fuel cells for portable applications. For example, DAFCs utilize liquid fuels, which increase the ease of handling and safety of the alcohol fuel. In addition, the energy densities of low molecular weight alcohols are higher than liquid hydrogen. In DAFCs, the alcohol molecule is directly oxidized on the anode, releasing protons and electrons. The electrons travel through an external circuit to the cathode side whereas the proton is transported through a proton exchange membrane (e.g., Nafion) to the cathode and reacts with the oxygen and electrons to produce water. Various alcohol molecules, such as methanol, ethanol, propanol, ethylene glycol, and glycerol, have been studied as fuels for DAFCs. However, to date, there are two major obstacles facing the development of DAFCs: (i) alcohol crossover from anode to cathode through the membrane and (ii) low activity and complex reaction mechanism of alcohol oxidation. In addition to this, the intermediates formed during the alcohol oxidation reaction, such as COads, poison the Pt catalysts.

Received: March 7, 2016  Accepted: May 3, 2016  Published: May 3, 2016
Methanol, being the simplest alcohol with no C–C bond, has been studied widely and has been shown to be able to completely oxidize to CO$_2$ giving 6e$^-$, but can also undergo multistep electron transfer reactions resulting in several reaction products and intermediates such as formaldehyde and formic acid. Higher alcohols which contain the C–C bonds are more difficult to oxidize as they form various adsorbed and intermediate species instead of completely oxidizing to CO$_2$, thus reducing the efficiency of the fuel cell. For example, on a Pt electrode in acidic media, within the fuel cell operating potential range, often the number of electrons obtained for CH$_3$CH$_2$OH (4e$^-$), HCHO (4e$^-$), HCOOH (2e$^-$), n-ProOH (4e$^-$), i-ProOH (2e$^-$), and ethylene glycol (4e$^-$) oxidation are lower than the theoretical e$^-$ yield for complete conversion to CO$_2$. Ethanol has been found to oxidize predominantly by 2e$^-$ and 4e$^-$ pathways to give acetaldehyde (AAL) and acetic acid (AA) as the major products, respectively. The reactivity of small primary alcohols have been observed to be in the order methanol > ethanol > propanol > n-butanol over Pt electrode in acidic media. Adsorbed CO formed as an intermediate during the alcohol oxidation, irreversibly adsorbs on Pt and acts as a catalyst poison, hindering further alcohol adsorption. Moreover, the removal of C$_2$, C$_3$, and C$_4$ intermediates formed during alcohol oxidation from the Pt surface is also a difficult process. Therefore, the complete oxidation of alcohol fuels to CO$_2$ is difficult to achieve, even with state-of-the-art Pt catalysts.

A general reaction of monoalcohol oxidation in acidic media can be written as in eq 1. Since an alcohol molecule contains only one oxygen atom, the complete oxidation to CO$_2$ requires an additional O atom, which is provided by the water or water adsorbed residue (OH$_{ad}$)$^+$ formed by water oxidation on Pt. However, the oxidation of water on Pt is a difficult process and requires a high potential which increases the anodic overpotential in DAFCs.

$$C_nH_{2n+1}OH + (2n - 1)H_2O \rightarrow nCO_2 + 6nH^+ + 6ne^-$$

(1)

It is clear from eq 1 that as the number of carbon atoms (n) increases, the number of e$^-$, which can be released during oxidation also increases (e.g., 6 e$^-$ per molecule for methanol to 24 e$^-$ per molecule for butanol). This makes longer chain length alcohol molecules, such as butanol, interesting fuel candidates for DAFCs. In addition, the alcohol crossover rate is expected to decrease with the alcohol chain length. Thus, by achieving a complete oxidation of the alcohol molecule at a lower potential, a high fuel cell efficiency could be achieved.

Various other factors such as availability, cost and sustainability also have to be considered, while selecting a suitable fuel for DAFCs. Although methanol is relatively facile to oxidation, it is toxic, flammable with low boiling point (65 °C) and is not a primary/renewable fuel and cannot be considered as an ideal fuel for practical DAFCs. In contrast, ethanol is nontoxic and can be produced by fermentation of sugars. However, the utilization of first generation biofuels produced from food-based biomass feedstock, such as bioethanol, have been the subject of significant debate over the ethics of utilizing food stock for fuel production instead of nutrition. An alternate renewable source, which does not compete with the food production, is required for a sustainable energy future. Thus, second generation biofuels are proposed to be produced from nonfood based biomass feedstock such as lignocellulose biomass (LCB) (e.g., corn stover and fiber, wheat and barley straw, switchgrass, miscanthus). The advantages of cellulose and lignin based feedstock are that they are abundant and can be considered as a waste product. In this regard, butanol is considered a second generation biofuel, with better infrastructure compatibility and higher energy density than ethanol and are superior to ethanol as a fuel itself or as a gasoline additive. Also, biobutanol is nonpoisonous, non-corrosive, biodegradable and does not lead to soil and water pollution.

Smaller chain alcohols, such as methanol and ethanol, have been widely studied as fuels for DAFCs and their electro-oxidation mechanism well documented. However, butanol has been much less studied. Higher alcohols have also been studied due to the interest in the adsorption and oxidation of these molecules. The oxidation of butanol isomers on various electrodes (Pt, Au, Pd and Rh polycrystalline electrodes) in alkaline media was studied by Lamy et al. They have observed that the two primary alcohols, n-butanol and iso-butanol, have a similar activity on Pt in alkaline media, whereas the secondary isomer behaves differently. The ter-butanol was found to be unreactive on all electrodes studied at room temperature. Similar behavior was also observed by the present authors over Pt in alkaline media. Since the activation of αC–H was generally identified as the initial step in the alcohol oxidation, the different behaviors of the butanol isomers were assumed to be caused by the inductive effect. A study on single crystal Pt electrode has shown that Pt(111) is the most active surface with lower poisoning, whereas Pt(100) and Pt(110) surfaces showed high poisoning during n-BtOH oxidation in alkaline media, and based on the activity the single crystal planes were classified as Pt(111) > Pt(110) > Pt(100) > Pt polycrystalline.

Bimetallic catalysts are generally found to be more active than the monometallic catalysts for alcohol oxidation reactions. This has been generally attributed to the bifunctional mechanism and/or ligand effect. In addition, the positive effect of PtSn toward CO oxidation has been well reported in literature. The addition of an oxophilic metal to Pt provides OH$_{ad}$ at a lower potential than that on pristine Pt, which helps the removal of the poisoning species, CO$_{ad}$, by oxidizing it to CO$_2$. To date, PtSn was found to be the best catalyst for the ethanol oxidation reaction in acidic media. It has been observed that nonalloyed Sn is more active in providing OH species at lower potential than the alloyed Sn, which assists in the CO$_{ad}$ poisoning removal. PtSn was highly selective toward acetic acid formation during ethanol oxidation, whereas Pt showed selectivity toward acetaldehyde at potentials lower than that for PtOH$_2$ formation. The CO adsorbate was found to form at lower potential on PtSn compared to that on Pt during ethanol oxidation, indicating that PtSn also activates the dissociative adsorption of ethanol. DFT calculations on the PtSn system for CO oxidation showed that the CO binds only to Pt but not on Sn, whereas OH$_{ad}$ preferentially adsorbs on the Sn sites confirming the bifunctional mechanism on PtSn.

González et al. reported that alcohols with H at β- carbon are readily oxidizable on PtSn electrode at lower potential than on pure Pt. They proposed that H abstraction from α and β carbon could lead to a stabilizing enol form which could then easily convert to aldehyde by the adsorbed water on Sn active sites. Zhou et al. studied the single cell performance of direct ethanol fuel cell using PtSn as the anode catalysts with various Sn content. All the PtSn catalysts studied (Pt,Sn/C, Pt3Sn2/C, Pt5Sn4/C, Pt9Sn7/C)
Pt$_2$Sn$_1$/C, Pt$_3$Sn$_1$/C, Pt$_4$Sn$_1$/C) showed a better performance than pure Pt, with Pt$_3$Sn$_2$ and Pt$_2$Sn$_1$ giving the maximum power density at 60 and 75 °C, respectively.

To the best of our knowledge, there are no reports on the comparison of the activity of butanol isomers on Pt in acidic media or on bimetallic catalysts. In this paper, attempt has been made to give insight into the activity of various isomers of butanol on Pt and PtSn catalysts in acidic media, building upon our previous reported data on $n$-BtOH over Pt and PtSn. Both electrodeposited PtSn and Sn-modified commercial Pt/C have been studied.

2. EXPERIMENTAL SECTION

Four different isomers, $n$-butanol (Alfa Aesar, 99.4%), 2-butanol (Aldrich, $\geq$ 99%), iso-butanol (Aldrich, $\geq$ 99%), and ter-butanol (Aldrich, $\geq$ 99%) were used as received without further purification. H$_2$PtCl$_6$·6H$_2$O (Alfa Aesar, $\sim 40$% Pt) and SnCl$_2$·2H$_2$O (VWR, AnalaR, NORMAPUR) were used for the catalyst preparation. All solutions were prepared using Barnstead Nanopure deionized (DI) water (resistivity 18 MΩ cm).

2.1. Synthesis of Carbon-Supported PtSn Catalysts. The carbon-supported PtSn catalysts were prepared by modifying the commercial catalyst HisPEC-4000 Pt/C (40 wt %) catalyst with Sn using the ethylene glycol (Alfa Aesar, 99%) reduction method. For this, about 300 mg of Pt/C (40 wt %) was dispersed in 30 cm$^3$ ethylene glycol (EG) by ultrasonication and to this, the required amount of SnCl$_2$·2H$_2$O was added to obtain the various mol % of Sn. The pH of the mixture was then adjusted to $\sim$11–13 by using 1 M NaOH (in EG) and the mixture was refluxed at 180–190 °C for 2 h. The mixture was then cooled to room temperature slowly. The catalyst was then filtered, washed with deionized water and dried overnight in a drying oven. The catalysts prepared are denoted as PtSn (1:2), PtSn (3:1), and PtSn (2:1) based on the mole ratios of Pt and Sn. An alloy PtSn (3:1) was also prepared by the same method for comparison. In this case, H$_2$PtCl$_6$ was used as the Pt precursor and Vulcan XC-72 carbon black was used as a support. The H$_2$PtCl$_6$ and SnCl$_2$ were dissolved together and added slowly to the EG solution containing Vulcan XC-72 followed by the heat treatment and drying as explained above.

2.2. Physical Characterization. The structure of the carbon supported PtSn catalysts was investigated by powder X-ray diffraction (XRD) utilizing a Panalytical X-Pert Pro with Cu Kα radiation ($\lambda$ = 1.5406 Å). The crystallite sizes of the catalyst particles were evaluated using Scherrer equation from the average of the crystallite sizes of Pt(111), Pt(200), and Pt(220) planes. The surface morphology and elemental composition were studied by transmission electron microscopy (TEM) coupled with energy disperse spectroscopy (EDS) using a JEOL JEM 2100 electron microscope. The samples for TEM were prepared by adding a drop of the catalyst suspension (prepared by the ultrasonically dispersing the catalyst in ethanol) onto a Cu grid and then evaporating the ethanol. The average elemental composition was calculated from about 4–5 EDS spectra. The particle size was calculated from the TEM images (average particle size of $<50–80$ particles) manually using ImageJ software.

2.3. Electrochemical Analysis. The electrochemical measurements were carried out in a three electrode cell using a potentiostat (SP240, Bio-Logic). An Ag/AgCl-3 M NaCl (BaSi, USA) (0.210 V vs SHE) and a Pt mesh (Goodfellow, UK) were used as reference and counter electrodes, respectively. All potentials are referred in this article with respect to Ag/AgCl-3 M NaCl unless specified otherwise. The cyclic voltammogram (CV) analyses were carried out in 0.1 M butanol isomer $+0.1$ M H$_2$SO$_4$ solution. N$_2$ gas was passed through the electrolyte solution for 15 min before carrying out the electrochemical
analysis. All electrodes were tested in the supporting electrolyte before testing in the butanol containing solution. The current values were normalized with the active area of Pt calculated from the hydrogen desorption area in the supporting electrolyte free from butanol.

The Pt was deposited on glassy carbon (GC) electrode (Goodfellow, UK) from 5 mM H2PtCl6 + 0.5 M H2SO4 solution at a deposition potential of +0.22 V. The electrochemical active area of Pt, \( A_e \) (in cm²) was calculated from the CV of Pt in sulfuric acid (SA) supporting electrolyte using eq 2 where \( Q_{Hi} \) is the charge for hydrogen desorption and \( Q_{Pt} \) is the charge required to oxidize a monolayer of hydrogen from Pt surface (0.21 μC cm⁻²). The current values in the CVs were normalized using \( A_e \) of Pt to give the specific current density.

\[
A_e = \frac{Q_{Hi}}{Q_{Pt}} \tag{2}
\]

The PtSn electrode was prepared by the Sn deposition onto Pt from a freshly prepared solution of 1 mM SnCl₂ + 0.5 M H₂SO₄ at a deposition potential of −0.21 V (the standard reduction potential of Sn(II)/Sn(0) is ∼ −0.35 V). The Sn coverage was calculated from the CV data obtained in the supporting electrolyte, that is, the difference in the hydrogen desorption charge before and after the deposition.

For each of the carbon supported catalysts, a catalyst ink was prepared by mixing 5 μg of the catalyst with 1.5 cm³ (ethanol + water) solvent and 20 μL NaFion solution (5 wt % solution). The latter served both as adhesive and proton conductor. The mixture was then ultrasonicated for 30 min and 10 μL ink was drop casted on to a GC electrode (7 mm diameter). The electrode was then dried at ambient temperature and electrochemical tests were carried out in the supporting electrolyte as well as in butanol containing solution.

3. RESULTS AND DISCUSSION

The CVs of Pt electrodes between the hydrogen evolution and oxygen evolution potential limits in 0.1 M H₂SO₄ showed characteristic features of Pt such as hydrogen adsorption/desorption region, double layer region, and Pt oxide formation/reduction processes (Figure 1).

3.1. Butanol Isomers in Acidic Media. In our previous study, the activities of butanol isomers oxidation on Pt and Pd electrodes were studied in alkaline media and the reactivities were observed to be in the order of n-butanol > iso-butanol > 2-butanol > tert-butanol. Herein, the activities are compared in acidic media for butanol isomer oxidation on Pt. Since the state-of-the-art fuel cells use acidic type NaOH electrolytes for butanol isomer oxidation on Pt. Since the state-of-the-art fuel cells use acidic type NaOH electrolytes, the butanol isomer oxidation mechanism was studied in alkaline media as well as in acidic media using in situ FT-IR, which indicated that the dissociative adsorption (dehydrogenation and C–H bond cleavage) of n-butanol occurs at the double layer region to form CO₂ and its further oxidation to CO₃ and (ii) the formation of an intermediate product species (without C–C bond cleavage), such as an aldehydic and carboxylic species (Scheme 1).22,38

![Scheme 1. General Mechanism of Alcohol Oxidation on Pt Electrode](image)

The dissociative adsorption was found to be the fastest reaction step, and generally occurs at lower potential, forming CO₂. A parallel path to give intermediate species occurs with consecutive dehydrogenation steps involving C–H bonds and O–H bonds. Since the C–C bond cleavage is energetically more difficult than the C–H bond cleavage, the mechanism predominantly follows the second pathway to form partial oxidation products such as aldehyde or acid. The oxidation of these intermediate species to CO₂ is difficult and is generally considered as the rate-determining step in the overall oxidation reaction to CO₂.5,38 In the case of butanol, C1, C2, C3, and C4 intermediate species could be formed during the oxidation.40

Li et al.4,37 observed the formation of CO₂ at E < 0.33 V and CO₃ at E > 0.43 V during n-butanol oxidation on Pt in acidic media using in situ FT-IR, which indicated that the dissociative adsorption (dehydrogenation and C–C bond cleavage) of n-butanol occurs at the double layer region to form CO₂ (eq 3), which is then further oxidized at potential where Pt oxide formed (>0.43) to produce CO₃(eq 5). \( \text{CHOH} \rightarrow \text{HCHO} \rightarrow \text{CO₂} \)

\[
\text{CH₃CH₂CH₂CH₂OH} + \text{Pt} \rightarrow \text{Pt} - \text{CO₂} + \text{CH₃CH₂CH₂H} + 2\text{H}^+ + 2\text{e}^- \tag{3}
\]

The CO₂ formed on the Pt blocks the active sites and inhibits further butanol adsorption.4 This was confirmed in the present study, by varying the anodic potential limit \( E_{\text{pass}} \) during the CV analysis of n-butanol oxidation (Figure 2). As the forward potential limit was increased, the reoxidation peak \( a \) current increases and the peak potential shifts slightly to more negative. This indicates that Pt surface was progressively...
Research Article

where Pt oxidation of these isomers occurs only at the potential region clearly seen from the \( n \) was attributed to the CO\(_2\) asymmetric stretch. A further peak at \( \sim 2343 \text{ cm}^{-1} \) also appears in the same potential range, which can be attributed to the CO\(_{\text{ads}}\) asymmetric stretch. A positive peak at \( \sim 3743 \text{ cm}^{-1} \) also appears at the same potential and both peaks increased with an increase in the potential, supporting the proposal that the CO\(_2\) was produced by the CO\(_{\text{ads}}\) oxidation with the assistance of OH\(_{\text{ads}}\). This is clearly seen from the \( n \)-butanol and iso-butanol CV, as the oxidation of these isomers occurs only at the potential region where Pt–OH\(_{\text{ads}}\) is formed (0.50–0.75 V in Figure 1 a and b). The poisoning was also confirmed using in situ FTIR analysis (Figure S2). At \( E \geq 0.50 \text{ V} \), a negative feature (associated with product) appears at \( \sim 2343 \text{ cm}^{-1} \) in the FTIR spectra, which was attributed to the CO\(_2\) asymmetric stretch. A further negative band at \( \sim 3743 \text{ cm}^{-1} \) also appears in the same potential range, which can be attributed to the OH\(_{\text{ads}}\) on Pt. It is noted that the OH\(_{\text{ads}}\) and CO\(_2\) peaks appear at the same potential and both peaks increased with an increase in the potential, indicating an increased consumption of water following the reaction shown in Equation 4. These results clearly validate the influence of OH\(_{\text{ads}}\) in the oxidation of alcohol molecule on Pt. Both pathways i and ii of Scheme 1 can thus occur at high potentials.

\[
P t + H_2 O \rightarrow P t + H^+ + e^- + P t OH_{ads} + H^+ + e^- \quad (4)
\]

\[
P t - CO_{ads} + Pt - OH_{ads} \rightarrow CO_2 + Pt + H^+ + e^- \quad (5)
\]

Both CO\(_{\text{ads}}\) oxidation and direct alcohol oxidation might contribute to peak \( a_1 \) for \( n \)-butanol and iso-butanol. The CO\(_{\text{ads}}\) oxidation to CO\(_2\) frees the Pt sites for further butanol adsorption which could then be oxidized to give intermediate species (peak \( a_2 \)). In ethanol oxidation, the second peak is attributed to the production of acetic acid/acetalddehyde, together with some CO\(_2\). This incomplete oxidation was also thought to be due to C–C bond cleavage being hindered when OH\(_{\text{ads}}\) is formed on Pt. Li and Sun observed both CO\(_2\) and butyric acid at potentials >0.43 V during \( n \)-butanol oxidation. However, the butyric acid was difficult to oxidized further to CO\(_2\) and most of the CO\(_2\) produced during \( n \)-butanol oxidation was thus assumed to originate from the dissociative adsorption of butanol (eq 3). At potentials >1.00 V, the Pt surface is covered by the oxide species (Equation 6) and leads to a decrease in the oxidation current (Figure 1 a–c).

\[
2Pt - OH_{ads} \rightarrow Pt - O + H_2 O + Pt \quad (6)
\]

The reduction of the oxide species during the NGPS allows the reoxidation of the intermediate species formed during PGPS, as well as the oxidation of the freshly adsorbed \( n \)-butanol, giving rise to peak \( a_2 \). It was reported that the reoxidation peak preferentially gives the partial intermediate product rather than CO\(_2\) for ethanol oxidation, as studied by Wang et al. using differential electrochemical mass spectrometry (DEMS). This was attributed to the poor C–C splitting rate in the potential region of peak \( a_2 \). The peak current for peak \( a_3 \) during PGPS was significantly lower than found for peak \( a_2 \) as well as \( a_1 \) indicating poor kinetics of \( n \)-butanol oxidation on Pt, that is, lower yield of CO\(_2\). It has been reported elsewhere that the anodic peak current decreases with increase in the carbon chain and the activities of primary alcohols were in the order of methanol > ethanol > propanol > \( n \)-butanol. In our previous study of butanol isomers in alkaline media, the primary isomers showed an increase in oxidation current just after the hydrogen desorption region, indicating the effect of OH\(_{\text{ads}}\) on the alcohol oxidation as the Pt surface was already covered by OH\(_{\text{ads}}\) in the hydrogen region in alkaline media. Also here, the ratio of the peak \( a_2 \) to peak \( a_1 \) is higher for \( n \)-butanol and iso-butanol compared to that for 2° alcohol, which could indicate that for 1°butanol isomers, the direct oxidation pathway of alcohol could be more prominent relative to the CO pathway. In alkaline media, the peak \( a_3 \) to peak \( a_1 \) ratio was significantly lower indicating direct alcohol oxidation pathway is less prominent. In alkaline media, kinetic factors may improve the efficiency of the CO route due to easy OH adsorption. This could decrease the direct oxidation of alcohol molecules, whereas the CO route will be unaffected. In order to make use of the fuel in a fuel cell, a complete conversion to CO\(_2\) has to be achieved by making the reaction mechanism preferentially follow the CO pathway at a lower potential. From the above results, it is clear that for primary alcohols, the CO pathway is less prominent but occurs at lower potential, whereas the partial oxidation pathway is dominant and occurs at higher anodic potential.

ACS Applied Materials & Interfaces

Figure 2. Effect of varying anodic potential limit on the CV of Pt/GC in 0.1 M BtOH + 0.1 M H\(_2\)SO\(_4\) at room temperature. The anodic potential limit varied from 0.5 to 1.3 V with 100 mV increment. The cathodic potential limit was fixed at −0.22 V. Scan rate 20 mV s\(^{-1}\).
research Article

During NGPS, which released the Pt sites free for further intermediates were oxidized and the reduction of Pt oxide intermediates such as COads.13,49,53 Thus, oxidation of 2-butanone formation region (< 0.35 V) compared to the first anodic peaks for ethanol (22.1 kJ mol−1) and 2-propanol (10.4 kJ mol−1) has been reported, indicating facile reaction kinetics for 2-butanone oxidation. This indicates that the long chain 2° alcohols can give better performance, even without C−C bond cleavage, but the complete oxidation to CO2 does not occur at lower potential as they follow the nondissociative pathway. On the other hand, for 1° alcohol, the partial oxidation occurs at high potential only as the CO formed by dissociative adsorption blocks the Pt sites at a lower potential.

The peak current of a1 can generally be correlated with the oxidation activity of the alcohol molecule. On the basis of this, it is clear that both 1° and 2° isomers on Pt in acidic media have a similar activity. 2-Butanol, on the other hand, showed a higher current for peak a1 than the 1° alcohol. However, the peak a1 for 2-butanol oxidation is associated with a partial oxidation reaction without involving C−C bond cleavage, which thus reduces the conversion efficiency of 2-butanol when used as fuel. Ter-butanol, show no activity for oxidation on Pt.

The activity of the butanol isomers for oxidation on Pt in acidic media can thus be given in the order 2-BtOH > n-BtOH > iso-BtOH > ter-BtOH.

Thus, it is clear that 1° isomers are potentially more active for oxidation to give completely oxidized product CO2 at a lower potential, but the CO2 production is inhibited by the poisoning species CO. The FTIR and CV analysis indicate that OHads is essential for the CO oxidation and to release Pt sites. Modification of the Pt-based catalyst to provide OHads at lower potentials has the potential to effectively oxidize the 1° alcohols to give CO2. This strategy, however, may not be relevant to 2-butanol, where the mechanism follows a different pathway at lower potentials without COads formation. The addition of oxophilic metals to Pt were reported to enhance the alcohol oxidation reaction.15,22 This was explained by the ability of the oxophilic metal to oxidize water at lower potential, providing OHads species in comparison to bare Pt, where a high overpotential is required for H2O oxidation (bifunctional mechanism). The activity for chemisorption of water for various metals are in the order Cu < Pd < Rh < Pt < Ru < Sn.58 As Sn is the most active metal for water decomposition, a PtSn bimetallic system was studied for butanol oxidation, herein.

3.2. PtSn Bimetallic Catalyst for Butanol Isomer Oxidation in Acidic Media.

In our previous study,53 a higher activity of PtSn than Pt for n-butanol oxidation in acidic media was reported. Here, the reactivity of PtSn for the electro-oxidation of all four butanol isomers was compared to Pt in acidic media. Sn was electrodeposited on Pt as described in the Experimental Section. The Sn, especially on the surface, is likely to be mostly present as oxide55 because of the exposure to atmosphere, as well as the charge transfer from Sn to Pt caused by the electronegativity difference between the two metal atoms.5,21,50,60

In contrast to the 1° butanol isomers, the 2° alcohol, 2-butanol, showed quite a different CV feature (Figure 1c). Two oxidation peaks were observed during PGPS and one oxidation peak during NGPS. The oxidation current increased just after the hydrogen desorption region during the PGPS, giving rise to a peak at ∼0.35 V (peak a2) and another peak at ∼1.00 V (peak a3). During NGPS, an oxidation peak was observed at ∼0.30 V (peak a3). The peak a1 could be attributed to the dehydrogenation of 2-butanol, whereas peak a2 could be due to the direct oxidation of 2-butanol.52 The hydrogen desorption region was not suppressed as much as n-butanol and iso-butanol, which indicates that the dissociative adsorption (C−C bond breaking) did not occur for 2-butanol to form strongly adsorbed intermediates such as COads.13,49,53 Thus, oxidation of 2-butanol occurs once the hydrogen is desorbed from the Pt species from 2° alcohol does not require water and thus direct oxidation can occur before the water oxidation occurs on Pt.57 Oxidation of 2-butanol to 2-butanone can occur as given in eq 7.

\[
\text{CH}_3\text{CH}_2\text{CH(OH)}\text{CH}_3 \rightarrow \text{CH}_3\text{CH}_2(\text{CO})\text{CH}_3 + 2\text{H}^+ + 2\text{e}^- \quad (7)
\]

During the NGPS, a reoxidation peak was observed, as in the case of n-BtOH and iso-BtOH, in a similar potential region and can be attributed to the reoxidation of the butanol molecule.38 On increasing the anodic potential limit, oxidation current peaks a1, a2, and a3 all increased for 2-butanol (Figure S3). A negative potential shift of the peak a3 was also observed, than the PtO2 and then the surface could be freed up for further fuel adsorption and oxidation. When the potential limit was lower than the PtO2 formation region (<<0.70 V), both peak a1 and a3 superimpose, indicating a reversible reaction, confirming the lack of poisoning of Pt electrode during 2-BtOH oxidation.49 As the potential was increased beyond the PtO2 region, the intermediates were oxidized and the reduction of Pt oxide during NGPS, which released the Pt sites free for further 2-butanol adsorption and oxidation. This resulted in the increased NGPS oxidation peak current density and also explained its peak potential shift. On Pt and Pd in alkaline media, 2-butanol showed a lower onset potential as well as multiple oxidation peaks during PGPS.11 But in contrast to acidic media, the oxidation current was significantly lower for 2-butanol in alkaline media in comparison to the 1° alcohols showing the influence of the electrolyte media on the oxidation mechanism for 2-butanol.

Ter-butanol did not show any reactivity toward oxidation and the CVs were similar to that of Pt in the acidic supporting electrolyte at room temperature (Figure 1d). However, a small improvement in the ter-butanol oxidation activity on Pt at high temperature in acidic media has been reported elsewhere.12 The inactivity of ter-butanol is anticipated, as no αC−H bond is present in ter-butanol which is the first step in the oxidation of alcohol molecules. A similar inactivity of ter-butanol was also observed in alkaline media on Pt and Pd.41 A lower activation energy of 2.1 kJ mol−1 for 2-butanol oxidation on Pt/C microporous electrode in acidic media (at the first anodic peak of ∼0.35 V) compared to the first anodic peaks for ethanol (22.1 kJ mol−1) and 2-propanol (10.4 kJ mol−1) has been reported, indicating facile reaction kinetics for 2-butanone oxidation. This indicates that the long chain 2° alcohols can give better performance, even without C−C bond cleavage, but the complete oxidation to CO2 does not occur at lower potential as they follow the nondissociative pathway. On the other hand, for 1° alcohol, the partial oxidation occurs at high potential only as the CO formed by dissociative adsorption blocks the Pt sites at a lower potential.

The peak current of a1 can generally be correlated with the oxidation activity of the alcohol molecule. On the basis of this, it is clear that both 1° and 2° isomers on Pt in acidic media have a similar activity. 2-Butanol, on the other hand, showed a higher current for peak a1 than the 1° alcohol. However, the peak a1 for 2-butanol oxidation is associated with a partial oxidation reaction without involving C−C bond cleavage, which thus reduces the conversion efficiency of 2-butanol when used as fuel. Ter-butanol, show no activity for oxidation on Pt.

The activity of the butanol isomers for oxidation on Pt in acidic media can thus be given in the order 2-BtOH > n-BtOH > iso-BtOH > ter-BtOH.

Thus, it is clear that 1° isomers are potentially more active for oxidation to give completely oxidized product CO2 at a lower potential, but the CO2 production is inhibited by the poisoning species CO. The FTIR and CV analysis indicate that OHads is essential for the CO oxidation and to release Pt sites. Modification of the Pt-based catalyst to provide OHads at lower potentials has the potential to effectively oxidize the 1° alcohols to give CO2. This strategy, however, may not be relevant to 2-butanol, where the mechanism follows a different pathway at lower potentials without COads formation. The addition of oxophilic metals to Pt were reported to enhance the alcohol oxidation reaction.15,22 This was explained by the ability of the oxophilic metal to oxidize water at lower potential, providing OHads species in comparison to bare Pt, where a high overpotential is required for H2O oxidation (bifunctional mechanism). The activity for chemisorption of water for various metals are in the order Cu < Pd < Rh < Pt < Ru < Sn.58 As Sn is the most active metal for water decomposition, a PtSn bimetallic system was studied for butanol oxidation, herein.

3.2. PtSn Bimetallic Catalyst for Butanol Isomer Oxidation in Acidic Media.

In our previous study,53 a higher activity of PtSn than Pt for n-butanol oxidation in acidic media was reported. Here, the reactivity of PtSn for the electro-oxidation of all four butanol isomers was compared to Pt in acidic media. Sn was electrodeposited on Pt as described in the Experimental Section. The Sn, especially on the surface, is likely to be mostly present as oxide55 because of the exposure to atmosphere, as well as the charge transfer from Sn to Pt caused by the electronegativity difference between the two metal atoms.5,21,50,60

DOI: 10.1021/acsami.6b02863
ACS Appl. Mater. Interfaces 2016, 8, 12859−12870

12864

ACS Applied Materials & Interfaces

Research Article
The morphology of the Pt was not modified significantly by the Sn addition and a spherical cauliflower type of morphology of Pt was preserved for PtSn, as reported in our previous study.33 The current density value for PtSn electrodes was normalized by the \( A \) calculated from the CV of PtSn in 0.1 M \( \text{H}_2\text{SO}_4 \). The composition of PtSn was difficult to determine from EDX and XRD analysis due to the low Sn coverages, and also, it is likely that not all the Sn is being present in crystalline form.21 Thus, the Sn coverage (\( \theta_{\text{Sn}} \)) was calculated using the electrochemical method from the difference in the hydrogen desorption charge before (\( Q_{\text{H}} \)) and after the Sn deposition (\( Q_{\text{Sn}}^{\text{H}} \)), as given in eq 8.21 This method also allows the determination of the active area without modifying the Pt−Sn surface before testing it in butanol solution. Suppression of the hydrogen desorption region, as well as an increased double-layer current for the PtSn (because of the oxide formation) electrode, is consistent with the presence of Sn on Pt (Figure S5). This method has been reported in literature to estimate the Sn coverage on Pt.21,33,35,59

\[
\theta_{\text{Sn}} = \frac{Q_{\text{H}} - Q_{\text{Sn}}^{\text{H}}}{Q_{\text{H}}} \tag{8}
\]

During the PGPS in \( \text{H}_2\text{SO}_4 \) (Figure S5), an oxidation peak appears with an onset potential of \( \sim0.15 \text{ V} \) and the peak potential at \( \sim0.50 \text{ V} \) for PtSn, indicating the oxidation of adsorbed Sn species by the dissociation of water on Sn.21,33,59 A small reduction peak at \( \sim0.35 \text{ V} \) could be attributed to the reduction of oxidized Sn, as at the upper potential in the CV, Pt surface is not oxidized.59 The upper potential in CV analysis was limited to a maximum of 0.60 V for PtSn to avoid dissolution of Sn into solution at higher potentials.61 The lower onset potential of tin oxidation (\( \sim0.15 \text{ V} \)) than the Pt oxidation potential (\( \sim0.55 \text{ V} \)) also confirms the oxophilic nature of Sn.

Figure 3a shows the PGPS of the Pt and PtSn electrode in 0.1 M \( n\)-butanol + 0.1 M \( \text{H}_2\text{SO}_4 \) solution. The Pt shows characteristic features of butanol oxidation with an onset potential of \( \sim0.55 \text{ V} \).\(^{33}\) However, for the PtSn electrode, a peak at lower potential of \( \sim0.27 \text{ V} \) was observed which is at significantly lower potential than the peak at \( \sim0.65 \text{ V} \) for Pt. Similar behavior was also observed for \( \text{iso-BtOH} \) (Figure 3 b). This lower potential peak was not observed in the supporting electrolyte (0.1 M \( \text{H}_2\text{SO}_4 \)), but only in \( n\)-butanol and \( \text{iso-BtOH} \) containing solutions, indicating that the peak originated from the butanol oxidation. This was also further confirmed by gradually adding \( n\)-butanol to 0.1 M \( \text{H}_2\text{SO}_4 \) supporting electrolyte while running the CV, the lower potential peak appears only when butanol was added to the solution (not shown). Since this peak appears at a potential region far below PtOH/PtO\(_x\) formation, the active oxygen species for the \( n\)-BtOH and \( \text{iso-BtOH} \) must originate from the Sn. The oxygenate species formed on Sn could be either an OH\(_{\text{ads}}\) species or the SnO\(_2\) itself.25 This may be attributed to the low onset potential for OH\(_{\text{ads}}\) formation on Sn as observed previously.25,62 A similarity between the primary butanol on PtSn and 2-butanol on Pt is notable. Both show an increase in oxidation current after the hydrogen desorption region, indicating that poisoning is not dominant and the oxidation
of the alcohol occurs in this potential region. A similar lower potential peak at \( \sim 0.23 - 0.29 \) V was also observed for ethanol oxidation on PtSn and methanol oxidation on PtRu.\(^{15}\) In addition to the lower onset potential, a higher current efficiency of CO\(_2\) production was also observed on PtRu and PtSn for the methanol oxidation reaction and was attributed to electronic modification of Pt by Ru in addition to the bifunctional mechanism.\(^{15}\) It is noted that the onset for n-butanol and iso-butanol oxidation on PtSn was at significantly lower potential (\( \sim 0.0 - 0.05 \) V) compared to that on Pt (\( \sim 0.55 \) V). A lower onset of 150–300 mV for CO oxidation on PtSn compared to Pt was observed in CO stripping experiments,\(^{25,26}\) confirming the positive effect of Sn on the CO oxidation reaction on Pt. Also, a lower onset potential of about 100–200 and 200–300 mV, respectively, for methanol and ethanol oxidation on PtSn compared to Pt has been reported and explained by the bifunctional mechanism. The Sn adsorbs oxygenated species at lower potentials leading to the easy removal of strongly adsorbed CO\(_{ads}\) as given in eq 9–12,\(^{25,26}\) which helps in the further adsorption of butanol. This is a significant observation as it indicates that even long chain alcohol, such as butanol, could be effectively oxidized on bimetallic PtSn catalyst, at even lower potential than ethanol on Pt electrode.

\[
\begin{align*}
SnO_2 + H_2O &\rightarrow SnO_2-OH_{ads} + H^+ + e^- \\
Sn + H_2O &\rightarrow Sn-OH_{ads} + H^+ + e^- \\
Pt-CO_{ads} + SnO_2-OH_{ads} &\rightarrow CO_2 + H^+ + e^- \\
Pt-CO_{ads} + Sn-OH_{ads} &\rightarrow CO_2 + H^+ + e^-
\end{align*}
\]

(9) (10) (11) (12)

The effect of temperature on n-butanol oxidation on electrodeposited Pt and PtSn electrodes was reported in our previous work\(^{33}\) and a lower activation energy on PtSn compared to Pt was observed at the oxidation peak region. González\(^{2}\) observed that alcohols with H atoms on the \( \beta \) carbon can be oxidized on PtSn at lower potential than on Pt. They proposed that H abstraction from \( \alpha \) and \( \beta \) carbons could lead to the formation of a stabilizing enol structure which could then convert to an aldehyde. This conversion would be facilitated by the O-rich surface of the Pt–Sn, as the attack on enol by adsorbed H\(_2O\) could easily form a hydrated aldehyde.\(^{3}\)

It was observed in our previous experiments on n-butanol oxidation that, at high Sn coverage (>40%), the anodic peak current at \( \sim 0.60 \) V was suppressed significantly\(^{33}\) and was assumed to be the blocking of Pt active sites by the Sn adatoms.\(^{33}\) However, with an increase in number of cycles between the potential ranges \(-0.22 \) to \( 0.75 \) V, the peak at \( \sim 0.60 \) V starts to appear, indicating that dissolution of Sn may be occurring at higher potentials, freeing up the Pt active sites for butanol adsorption. It is obvious that the Pt active sites are required for the butanol adsorption as Sn does not adsorb CO\(^{34}\) but only helps in the water adsorption at low overpotentials.\(^{21}\)

The PtSn electrode for the oxidation reaction of iso-butanol also showed a similar feature to that of n-butanol (Figure 3b), whereas 2-butanol and ter-butanol did not show any significant activity on the PtSn electrode. As discussed previously for the Pt electrode, CO\(_{ads}\) was not formed from 2-butanol and thus no significant improvement was observed on PtSn compared to Pt. Similar behavior was also observed for 2-propanol oxidation on PtRu with no difference in the activity compared to pure Pt.\(^{52}\)

The inactivity of ter-butanol on PtSn has also been reported.\(^3\) As discussed in the previous section, the primary isomers of butanol are more active for the oxidation reaction, but the CO poisoning increases the overpotential. It was clear from this study that using bimetallic catalyst such as PtSn, the poisoning species can be removed at lower potential and thus can facilitate the oxidation of butanol at a lower potential.

3.3. Carbon-Supported PtSn Catalyst for \( n \)-Butanol Oxidation. To further confirm the Sn effect on Pt for butanol oxidation, and also to control the Sn composition more accurately, commercial Pt/C (40%) was modified by Sn using a chemical reduction method described in the Experimental Section. The XRD spectra of the PtSn/C catalysts are given in Figure 4. The XRD shows typical peaks for the face centered cubic (fcc) structure of crystalline Pt.\(^{53}\) The particle size of Pt was in the range of \( \sim 4.1 - 4.4 \) nm for all the samples and was calculated using the Scherrer equation.\(^{34}\) Only PtSn with high Sn content showed Sn related peaks in the XRD which were not observed at low Sn contents.\(^{32}\) For the higher Sn loaded materials, two peaks with the 2\( \theta \) at \( \sim 34^\circ \) and \( \sim 53^\circ \) were observed which may be associated with the SnO\(_2\) phase.\(^{53-65}\) However, these peaks were relatively broad, which could indicate the amorphous nature of Sn as the catalysts were used as prepared and not subjected to further heat treatment.

For the PtSn (3:1)-alloy catalyst, all the diffraction peaks were slightly shifted to lower 2\( \theta \) values compared to the Pt/C (40%), which confirm alloy formation,\(^{5,25}\) whereas for all other Sn-modified Pt/C catalysts, no such peak shifts were observed, confirming the nonalloy nature of the PtSn particle, as expected. Also the particle size for the alloy was lower than that of the Sn modified Pt/C catalysts, which is typical for alloy catalysts.\(^{25}\) The BET surface areas of these catalysts were not significantly different after Sn addition, although a slight increase in the surface area was observed with increase in Sn content for the PtSn/C catalysts (Table 1). The alloy catalyst, on the other hand, showed a higher surface area than all other catalysts, which may explain the slightly greater current density associated with the PtSn(3:1) alloy catalyst (Figure S6) compared to the Sn modified PtSn(3:1) catalyst.

The TEM images of the PtSn(3:1) and PtSn(2:1) are given in Figure S5. A uniform distribution of the spherical particles on the carbon support is evident from the TEM. The average
Table 1. Physical Properties of the PtSn Nanoparticle Catalysts Studied

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>Sn (mol %) theoretical</th>
<th>Sn (mol %) from EDX</th>
<th>Average crystallite size of Pt from XRD (nm)</th>
<th>BET surface area (m² g⁻¹)</th>
<th>Average particle size from TEM (nm)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Pt/C (40%)</td>
<td>0</td>
<td>3.7</td>
<td>140</td>
<td></td>
<td></td>
</tr>
<tr>
<td>PtSn (1:2)</td>
<td>66.6</td>
<td>68.5</td>
<td>4.1</td>
<td>143</td>
<td>3.0</td>
</tr>
<tr>
<td>PtSn (2:1)</td>
<td>33.3</td>
<td>36.5</td>
<td>4.4</td>
<td>143</td>
<td>4.2</td>
</tr>
<tr>
<td>PtSn (3:1)</td>
<td>25</td>
<td>24.5</td>
<td>4.4</td>
<td>134</td>
<td>3.2</td>
</tr>
<tr>
<td>PtSn (4:1)</td>
<td>20</td>
<td>23</td>
<td>4.4</td>
<td>133</td>
<td>3.5</td>
</tr>
<tr>
<td>PtSn (3:1) alloy</td>
<td>25</td>
<td>25.4</td>
<td>3.6</td>
<td>159</td>
<td>3.9</td>
</tr>
</tbody>
</table>

Crystalite size was calculated from the average of the crystallite size of Pt(111), Pt(200) and Pt(220) planes. Sn mol % calculated from the average of 4–5 EDS spectra.

Figure 5. TEM images of (a, b) PtSn(3:1)/C and (c, d) PtSn (2:1)/C nanoparticles.

Particle size from TEM and XRD was similar, with a slightly higher value obtained from XRD. This could be due to the fact that the TEM particle size was calculated from the average 50–80 clearly distinguishable particles, whereas XRD represents the bulk sample and the response is dominated by the large crystallites present. An EDS analysis was also carried out for the TEM samples and the compositions obtained for the various samples are given in Table 1. The composition obtained was more or less similar to that expected. However, the possibility of some Sn being deposited on carbon cannot be discarded.

The PGPS voltammogram of PtSn/C nanoparticles in n-butanol-containing solution is compared in Figure 6. For all PtSn catalysts, an oxidation peak between 0.1–0.3 V was observed as found for the electrodeposited PtSn catalyst in Figure 3. However, the current density was found to vary with the composition of the catalysts. The maximum current density for the lower potential peak was found for PtSn(3:1). This could be the result of the Pt active sites being blocked by excess Sn for butanol adsorption at higher Sn contents, whereas, at lower Sn content, there was not sufficient OHads species on Sn sites for COad oxidation. Thus, it may be assumed that there is an optimum Sn coverage required for an effective butanol oxidation. The PtSn electrodeposited catalyst also showed a higher current for ~25% coverage and thus about 20–30% Sn could be considered as an optimum Sn content for the PtSn catalyst. The PtSn(3:1)-alloy catalyst also showed a clear lower potential peak (Figure S6), confirming this assumption. A slightly higher peak current was observed for PtSn(3:1)-alloy catalyst (Figure S6) compared to the nonalloyed catalyst (Figure 6b), which is in contrast with some of the previous reports, where poor activity has been observed for alloy PtSn catalysts, and had been attributed to the electronic interaction between Pt and Sn in the alloy phase. On the contrary, the electronic effect can also be advantageous, as the charge transfer to Pt by Sn can weaken the Pt-CO bond, which helps in the removal of CO as to be oxidized to CO₂.67,68 Silva et al.99 observed a higher current density during ethanol oxidation for PtSn/C alloy catalyst compared to the nonalloyed one which was attributed to the CO₂ formation with slow kinetics on nonalloyed catalyst vs acetic acid formation with faster kinetics for alloyed catalyst. However, as mentioned before the higher surface area could also be the reason for the higher current in the case of alloy catalyst. Further studies are required to clearly distinguish the difference in activity/mechanism in alloy and nonalloyed catalyst.

The Arrenhius plots of the butanol oxidation on Pt/C (40%) commercial catalyst and PtSn(3:1) are given in Figures S7 and S8. The activation energy for n-butanol oxidation on PtSn(3:1) at 0.20 and 0.30 V was significantly lower (15 kJ mol⁻¹) than found for Pt/C (40%) at 0.62 V (37 kJ mol⁻¹). Similar results were also observed for electrodeposited PtSn in our previous study.33 Since the first peak on Pt is attributed to the butanol oxidation after the removal of COad species, the lower activation energy on PtSn can be attributed to the effectiveness of the catalyst in COad removal by the bifunctional mechanism which helps in the adsorption of butanol molecules on Pt. An increase in the lower potential oxidation peak current with increase in n-butanol concentration was observed for PtSn(3:1)/C (Figure S9). Also, with increase in the BtOH concentration, the peak becomes more distinguishable at higher BtOH concentration. A similar behavior was also reported for ethanol oxidation reaction on PtSn.70 All of these confirm the fact that the lower potential peak originates from the butanol oxidation reaction.

4. CONCLUSIONS

A series of long chain C₄ alcohols have been studied for electrochemical oxidation in acidic media on a Pt electrode. It was demonstrated that the different butanol isomers behave differently in their electrochemical oxidation. Both 1° alcohols, n-butanol and iso-butanol, have a similar reactivity for oxidation, whereas 2-butanol, a 2° alcohol, is quite different in its electrochemical oxidation behavior. This indicates a difference in the mechanism of the 1° and 2° isomers. From the CV and FTIR results, it was proposed that 2-butanol does not undergo C–C bond cleavage and thus not produce poisoning species such as COad. The oxidation current was also higher for 2-butanol compared to that of 1° alcohols, indicating its effectiveness in oxidation without C–C cleavage to give partial oxidation products, though the partial oxidation will reduce the conversion efficiency of the fuel. The ter-butanol, on the other hand, is not reactive for oxidation at all. The 1° and 2° isomers
of butanol showed a similar current density, indicating a similar reactivity in acidic media; whereas in alkaline media the activity of 2° isomers was lower than that of 1°, as reported in our previous study. Thus, in both media, primary butanol isomers could be considered as suitable fuels for DAFCs. In addition, both the 1° butanol isomers can be produced from biomass which makes them an attractive fuel for a sustainable energy future. The in situ FTIR data provides evidence of the effect of OH_ads in removing CO_ads, and it was concluded that the OH_ads is essential in the oxidation of alcohol on Pt.

To reduce the CO_ads poisoning effect by forming OH_ads at a lower potential, PtSn bimetallic catalysts/electrodes were studied, and a significant improvement in the performance was observed for the 1° isomers of butanol, with an oxidation peak at ≈0.25–0.30 V which is at a significantly lower overpotential than that on bare Pt. However, no significant effect with Sn addition to Pt was observed for 2° and 3° butanol. The higher activity on Sn addition to Pt for the 1° butanol could be attributed to the bifunctional mechanism associated with the bimetallic electrode. The higher activity for PtSn was also confirmed for carbon supported PtSn nanoparticle catalysts prepared by modifying commercial Pt/C with Sn. The peak at lower potential was also present in the PtSn/C electrode and a high activity was observed for PtSn(3:1)/C catalyst. The activation energy for butanol oxidation was also observed to be lower on PtSn(3:1)/C (∼15 kJ mol⁻¹) compared to that of Pt/C catalyst (∼37 kJ mol⁻¹).

Overall, we have successfully demonstrated that higher alcohols, especially bio-butanol, have the potential to be used as fuel for DAFCs, especially on multifunctional catalysts such as PtSn. Nevertheless, a detailed further study is ongoing regarding the oxidation mechanism of butanol over bimetallic catalysts which will help in the further development of multifunctional catalysts for complete electro-oxidation of bio-butanol.

**ASSOCIATED CONTENT**

*E-mail: w.lin@lboro.ac.uk.*

*E-mail: c.hardacre@manchester.ac.uk.*

The authors declare no competing financial interest.
UK Catalysis Hub is kindly thanked for resources and support provided via our membership of the UK Catalysis Hub Consortium and funded by EPSRC (Grant no. EP/K014706/1). Material Chemistry Centre, Dept. of Chemistry, UCL, and Dr. Ana Jorge Sobrido, Dept. Of Chemical Engineering, UCL, are kindly acknowledged for their help and support in the TEM analysis.

REFERENCES

(33) Puthiyapura, V. K.; Brett, D. J. L.; Russell, A. E.; Lin, W. F.; Hardacre, C. Development of a PtSn Bimetallic Catalyst for Direct


